

Oxycodone, A 100-year old Synthesis: Continuous Flow *vs.* Batch Process

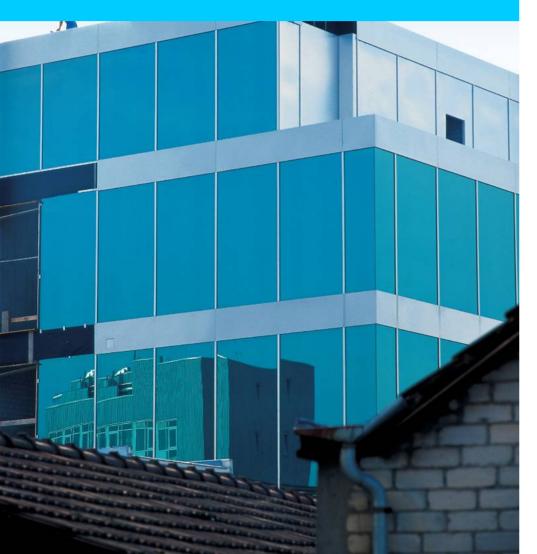
RSC Symposium – Continuous Flow Technology Geneva, June 16, 2011 Beat Weber





- Introduction
- Chemical Background
- Proposed Approach
- CFT Application (Feasibility)
- CFT Optimization
- Achievements

Overview Profile

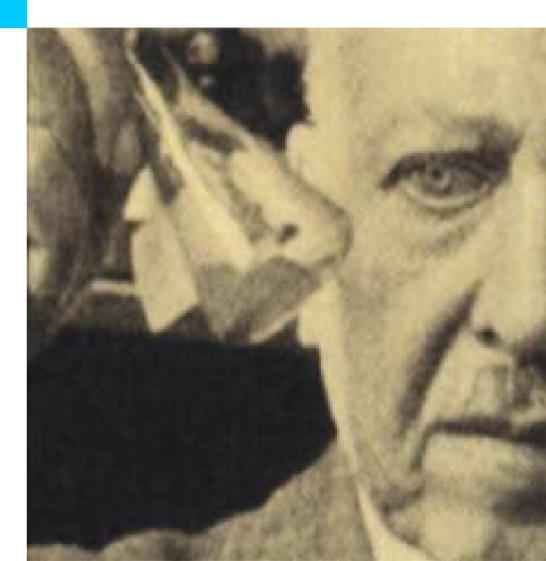


- Globally focused
- Independent
- Listed on the Swiss Stock Exchange (SIX)
- Concentration on the development and manufacturing of active pharmaceutical ingredients (API) and intermediates, as well as drug products
- Total work force: approx. 700
- Annual sales CHF: approx. 314 mio

Siegfried at a glance

Overview Past to present

- 1873 Pharmacist Samuel BenoniSiegfried founds a company with12 employees as a supplier topharmacies
- 1904 Conversion into a joint stock corporation
- 1937 Founding of Ganes Chemical Works, Inc. (NJ, USA)
- 1973 Quotation on the Swiss Stock Exchange (SWX) in Basel
- 1991 Focus on development and custom manufacturing
- 2001 Building of two core divisions: Siegfried and Sidroga



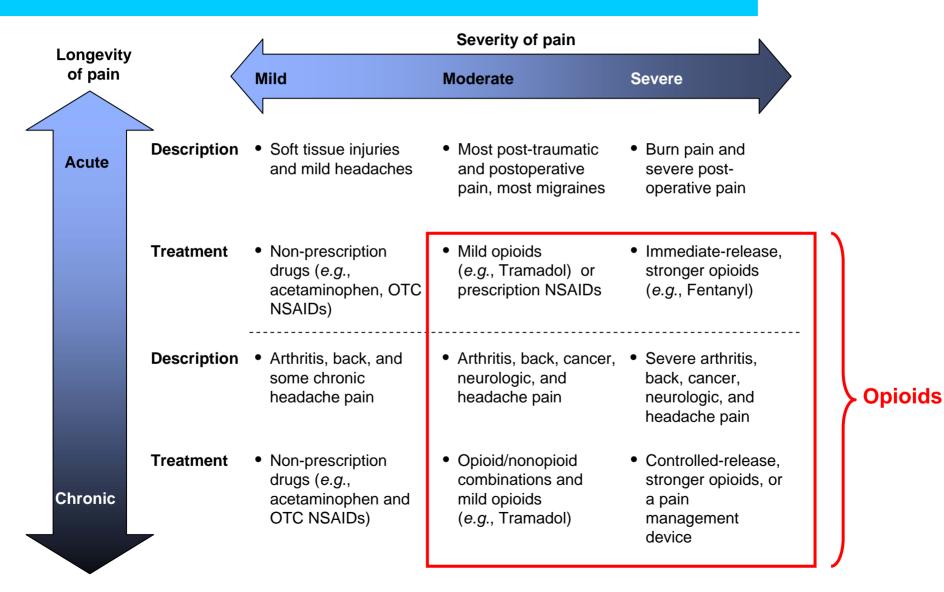
Overview Our Vision

To be a world-class service partner in developing and manufacturing drug substances and drug products that improve human life.



Introduction The pain treatment landscape

Siegfried

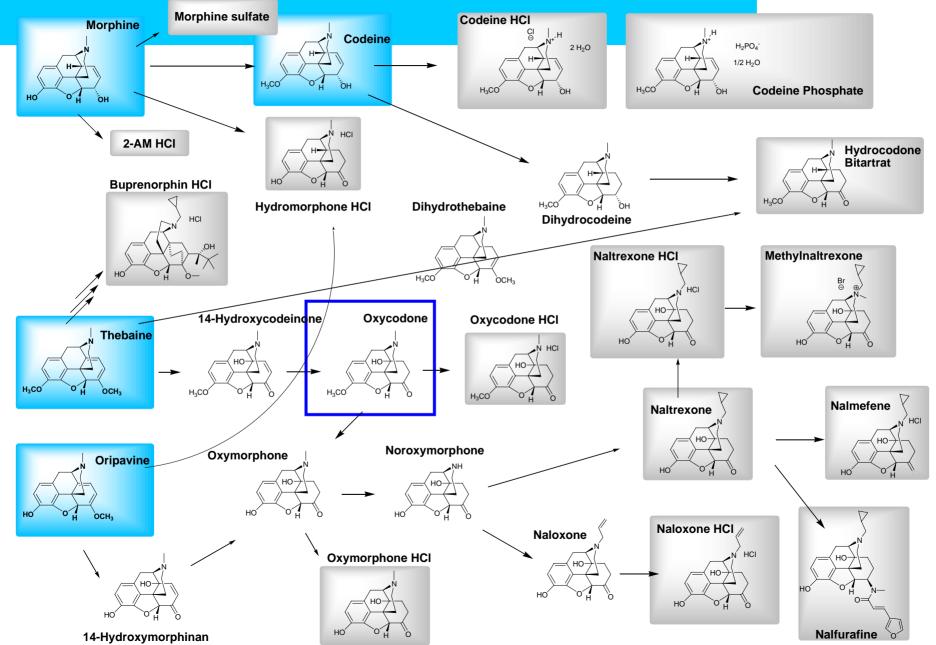


SOURCE: Team analysis

	Name	Relative Potency	Classification
Strong Opioids	Sufentanil	~1000	Agonist
	Fentanyl	120	Agonist
	Buprenorphine	~30	partial Agonist
	Hydromorphone	7,5	Agonist
	Oxymorphone	7	Agonist
	Oxycodone	1,5 – 2	Agonist
	Methadone	2	Agonist
	Hydrocodone	1,5	Agonist
	Morphine	1	Agonist
Mild Opioids	Pentazocine	0,3	mixed Agonist-Antagonist
	Codeine	0,2	Agonist
	Pethidine	0,1	Agonist
	Tramadol	0,1 – 0,2	Agonist
	Tilidine	0,1 – 0,2	Agonist

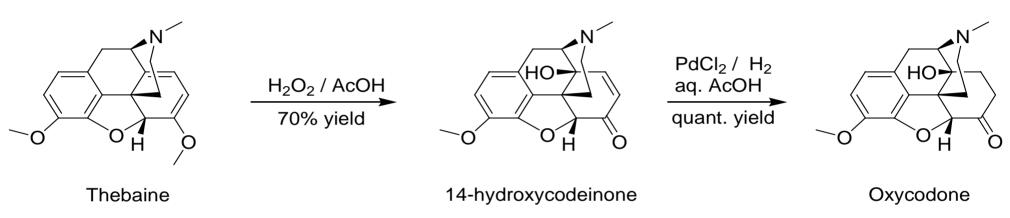
Introduction – The opiates family tree





Introduction Early Findings by Freund & Speyer

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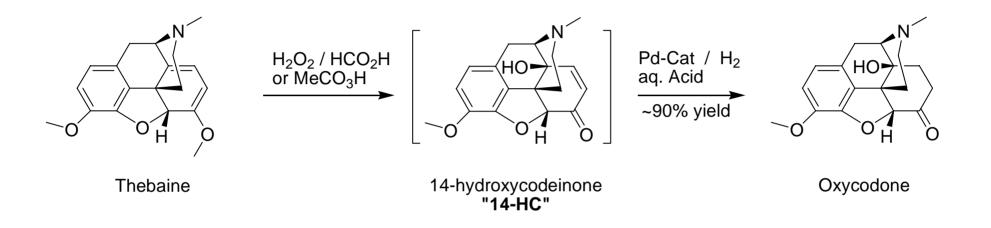


Die neuen Verbindungen sollen als Arzneimittel Verwendung finden.

Source: Chem. Zentralbl. 1915, <u>94</u>, 156,157; DE296916 (1916); DE286431 (1914)

Introduction Current Synthesis used by the Industry

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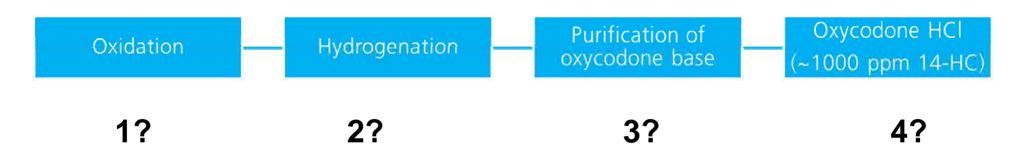


Still, more or less, the same route and conditions as Freund & Speyer

New challenge: Regulatory authorities limit 14-hydroxycodeinone to not more than 10 ppm for pharmaceutical purposes

Introduction Adapt / Change the Current Process

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Modify the batch process to get product with 10 ppm level of 14-HC:

- **1** Apparently not relevant: oxidation product is **14-HC**
- 2 Seems to be attractive as 14-HC is transformed into oxycodone
- 3 Typical up-grade / purification approach
- 4 Typical up-grade / purification approach

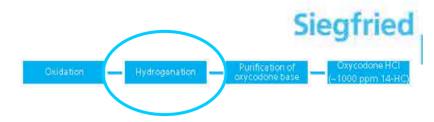
Introduction Adapt / Change the Current Process Siegfried Oxidation Hydrogenation Purification of oxycodone base Oxycodone HCl (~1000 ppm 14-HC) 1? 2? 3? 4?

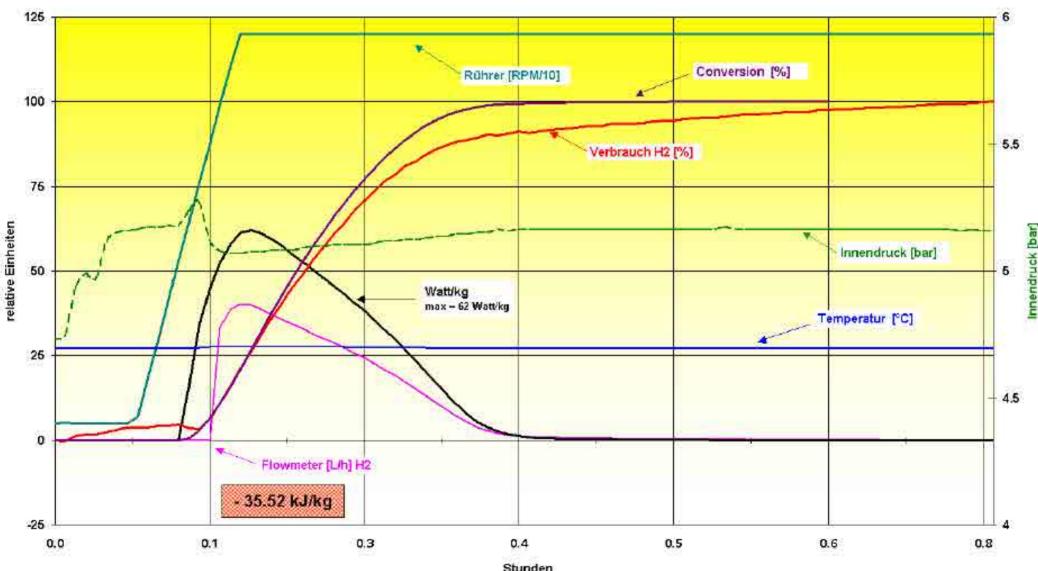
Purity up-grade approach was tested first with limited success:

14-HC can only be removed by processes associated with huge product losses



Chemical Background Hydrogenation Step (2)





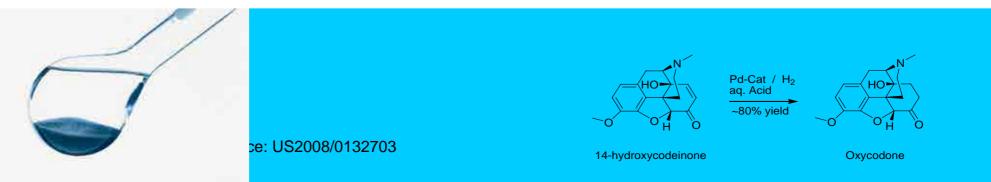
Hydrogenation runs smoothly

- In-process monitoring shows complete consumption of 14-HC (~10 ppm)
- Nevertheless, the product is contaminated with 500 to 1500 ppm 14-HC
- A second hydrogenation, with purification, removes the 14-HC to \leq 10 ppm, but the trade off is product loss.



Chemical Background Hydrogenation Step (2) – What's the Culprit?

ΉΟ■ HO. Ω + H₂O H_2O OH "Dihydroxy by-product" is HO• carried over to oxycodone, where it forms again 14-HC С upon synthesis and storage 6-Hydoxycodeinone



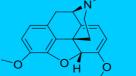
Chemical Background Challenges at the Hydrogenation Step (2)

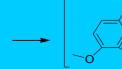
- A single hydrogenation step is desired –repeated hydrogenations are too expensive
- After hydrogenation, the level of 14-HC plus dihydroxy by-product must be < 50 ppm in the isolated base, to assure production of USP grade Oxycodone HCI

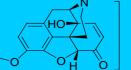


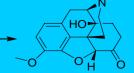
- Select an efficient hydrogenation catalyst – not sufficient
- Suppress formation of the dihydroxy by-product









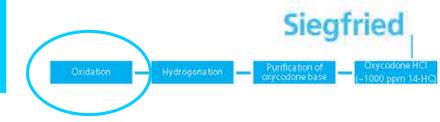


Thebaine

14-hydroxycodeinone

Oxycodone

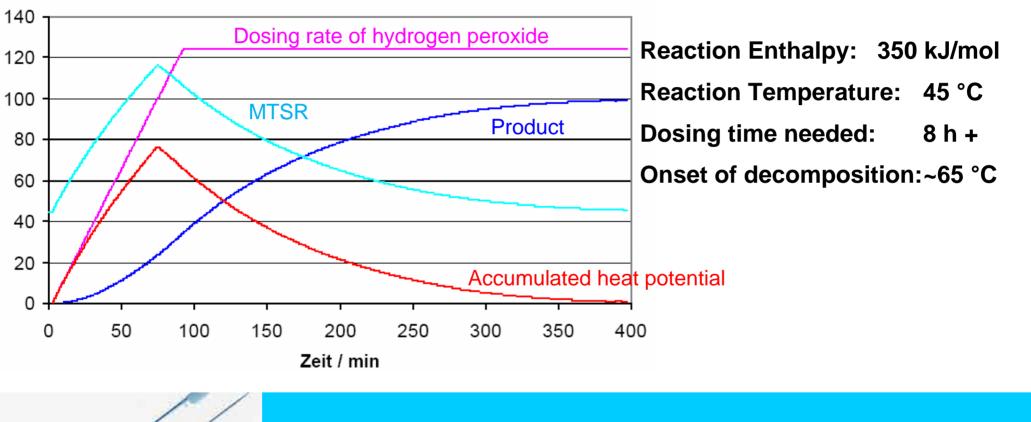
Chemical Background Oxidation Step (1): Heat-Flow Regime



H₂O₂ / HCO₂H

14-hydroxycodeinone

Thebaine

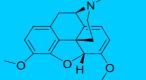


Chemical Background Challenges at the Oxidation Step (1)

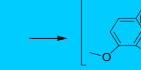
- Desired reaction is slow
- Reaction temperature is close to the decomposition temperature
- Reaction needs water (hydrolysis of ether)
- Undesired side reaction needs water
- Formation of the dihydroxy by-product is faster in the presence of peroxides
- Unreacted thebaine will also form byproducts; at most, 2% thebaine can be tolerated in 14-HC
- Suppress formation of the dihydroxy by-product

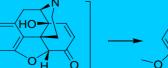
- Add a catalyst
- Tighten temperature control
- Need to compromise
- Control stoichiometry and quench quickly
- Push the reaction to not less than 98% conversion
- ?





Thebaine







14-1

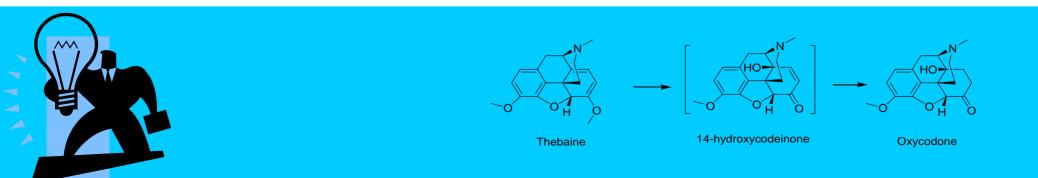
14-hydroxycodeinone

Oxycodone

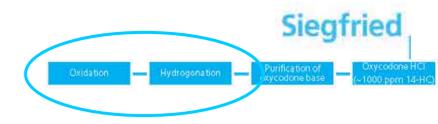
Proposed Approach

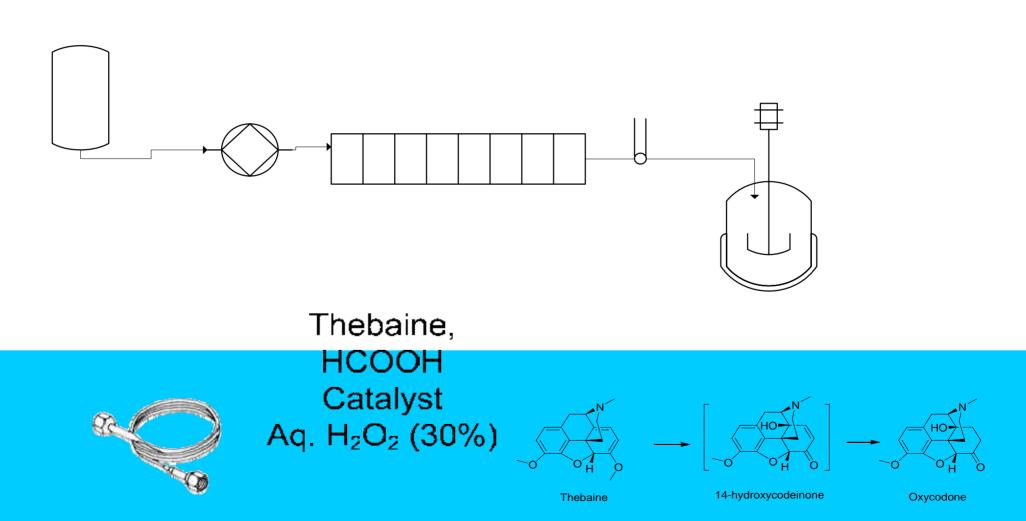


- Add a catalyst during the oxidation to form the peracid faster try phosphoric acid
- Run the oxidation in a well-defined temperature / time domain
- Start hydrogenation immediately after the oxidation step
- \rightarrow Continuous flow reaction for step 1
- \rightarrow Develop PAT monitoring for oxidation step
- \rightarrow Hydrogenate without delay



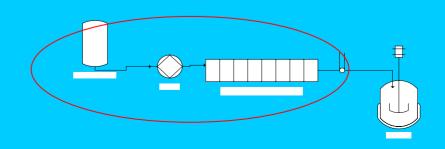
CFT Application (Feasibility) Approach for Initial Tests





- Phosphoric acid works as the catalyst
- Catalyst offers no advantage when the temperature exceeds ~60 °C
- Thermal reservoir (dilution) can be minimized within the CFT process
- At 100 °C, the reaction time is 2 3 minutes for > 98% conversion
- At 100 °C / 3 min, some unknown by-products can be tolerated (< 2%)





CFT Application (Feasibility) Oxidation Step – PAT Monitoring (Raman)

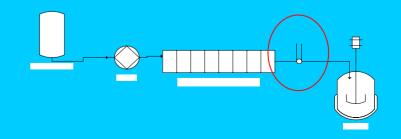
Raman Shift (1/cm)



n

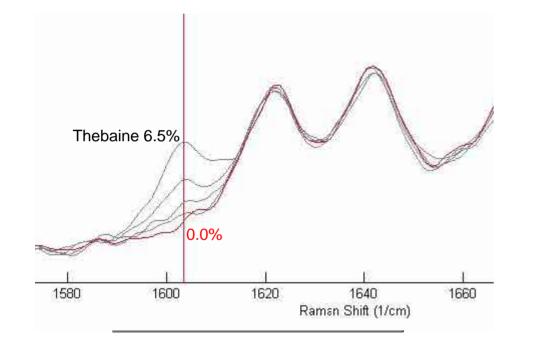
-2000

Counts

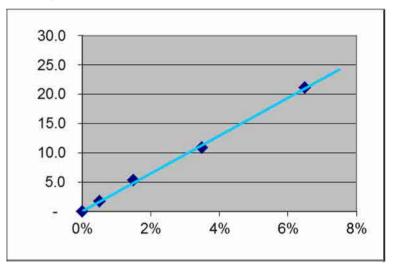


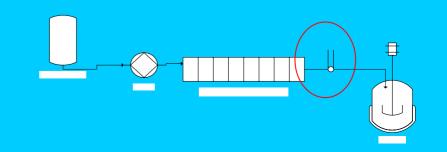
CFT Application (Feasibility) Oxidation Step – PAT Calibration (Raman)

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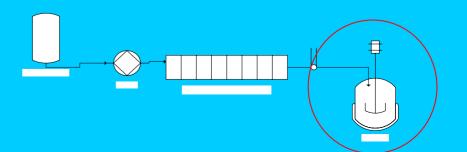
Signal vs. Unreacted Thebaine





- The reactor contains hydrogen gas and a precious-metal catalyst
- Excess peroxide may form oxygen, and create an explosive mixture
- \rightarrow Absence of peroxide confirmed at the outlet of the CFT unit
- → Palladium catalyst selected does not decompose peroxide to oxygen





CFT Application Plant Simulation – Initial CFT Set-Up

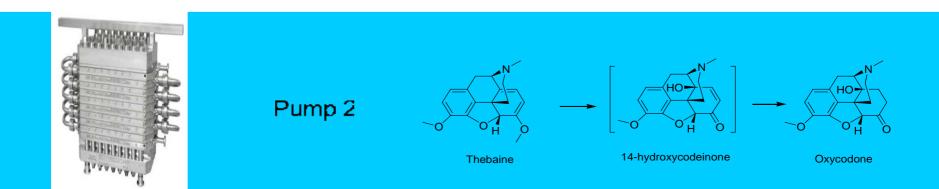
Thebaine, HCOOH Catalyst

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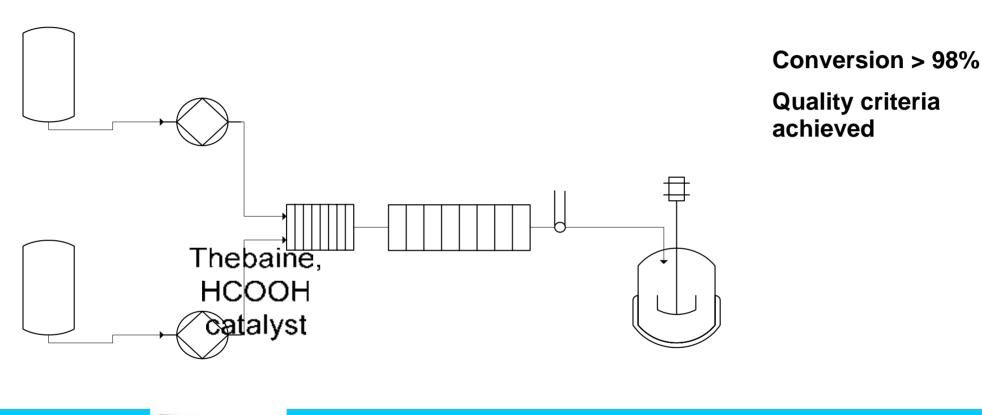
Conversion < 98%

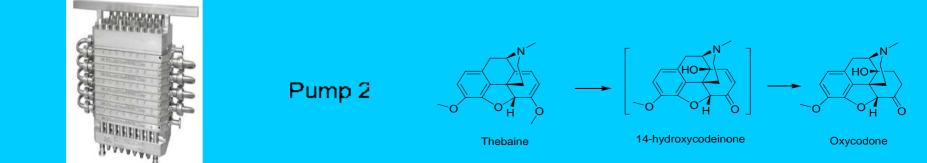
More by-products

Changing stoichiometry failed to optimize the reaction



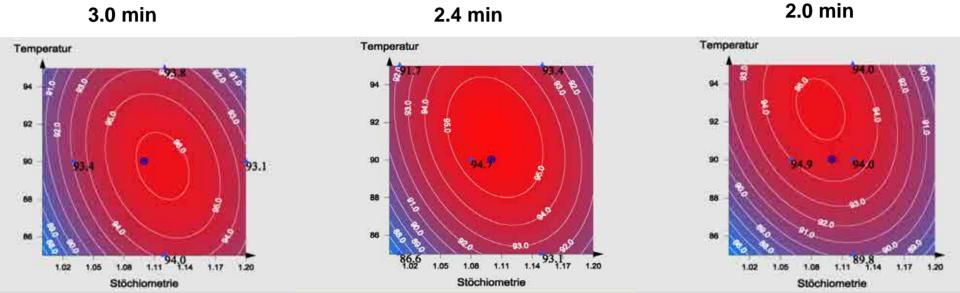
CFT Optimization Plant Simulation – Modified CFT Set-Up





CFT Optimization Design Space for Oxidation Step (1)

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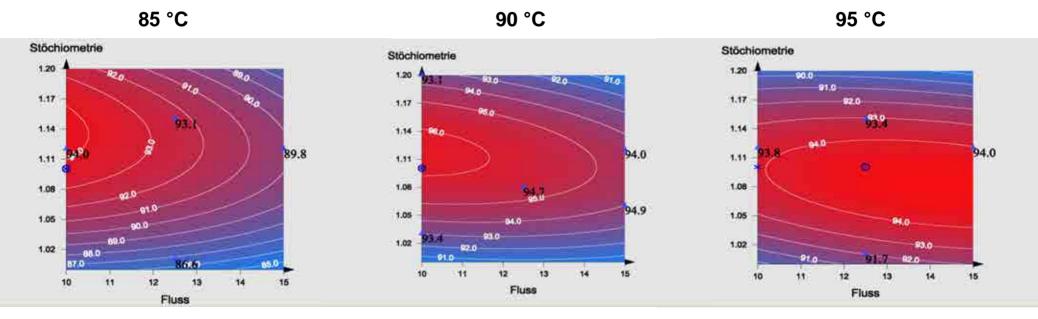


> Optimum residence time is 2.4 min

2.4 min

CFT Optimization Design Space for Oxidation Step (1)

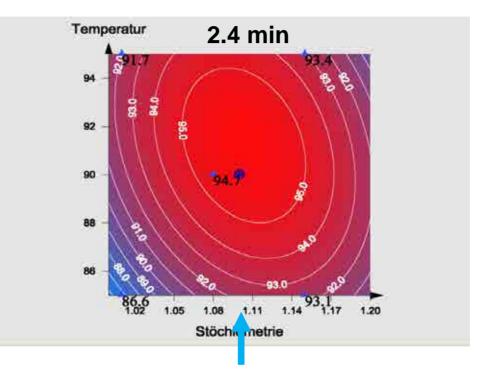
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> Optimum reaction temperature is 92 °C (with a residence time of 2.4 min)

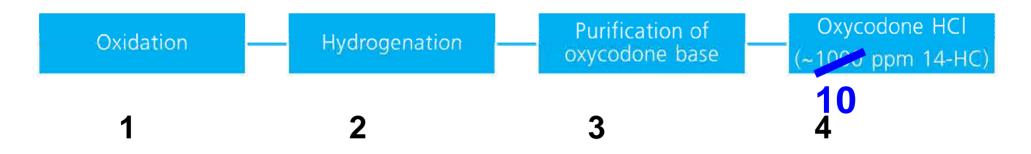
CFT Optimization Design Space for Oxidation Step (1)

Siegfried



> Optimum stoichiometry is 1.1 equivalent of hydrogen peroxide

Achievements Adapt / Change the Current Process



- $1 \rightarrow$ do the oxidation step continuously
- $2 \rightarrow$ run the hydrogenation more concentrated
- $3 \rightarrow$ simplify the existing purification protocol
- 4 \rightarrow use the existing salt formation process

Achievements Comparison of CFT with Batch Processes

	Original batch process	Modified batch process	CFT process
Stages	 Oxidation Reduction – isolation of oxycodone base Purification of oxycodone base Formation of Oxycodone HCI 	 Oxidation Reduction – isolation of oxycodone base Purification of oxycodone base Re-hydrogenation – isolation of oxycodone base Formation of Oxycodone HCI 	 CFT process– isolation of oxycodone base Formation of Oxycodone HCI
Batch cycle time		+ 33%	- 33%
Level of 14-HC	1000 ppm	10 ppm	10 ppm

- Cycle time shortened \rightarrow shorter lead time \rightarrow less net working capital
- Stringent quality attribute achieved without extra purification steps
- Inherent process safety is built in, and PAT capability easily installed
 - \rightarrow minimization of failed batches
- Siegfried plans installation of a 3-liter reactor, with a capacity of 20 MT/year



Thank you

- Stefan Sahli
- Vinzenz Blum
- Etienne Trachsel
- Roland Eberli
- Bernhard Berger
- Alexander Franz
- Orrin Viele III Chemistry
- Michael Levis

CFT CFT CFT

- Analytics
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