

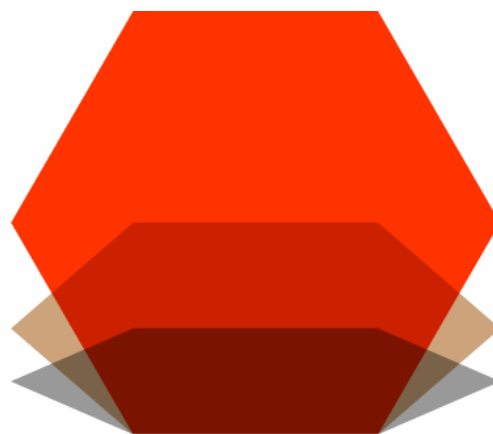


Your Specialist for Hazardous Reactions.



RSC Symposium - Continuous Flow Technology
Palexpo, Geneva, 15 -16 June 2011

Continuous Processes of Hazardous Reactions
from Lab to Commercial Scale



dottikon

EXCLUSIVE
SYNTHESIS

Your Specialist for Hazardous Reactions.

Continuous Processing at DOTTIKON EXCLUSIVE SYNTHESIS

Introduction

Batch vs. Continuous

Development and Realization of Continuous Processes

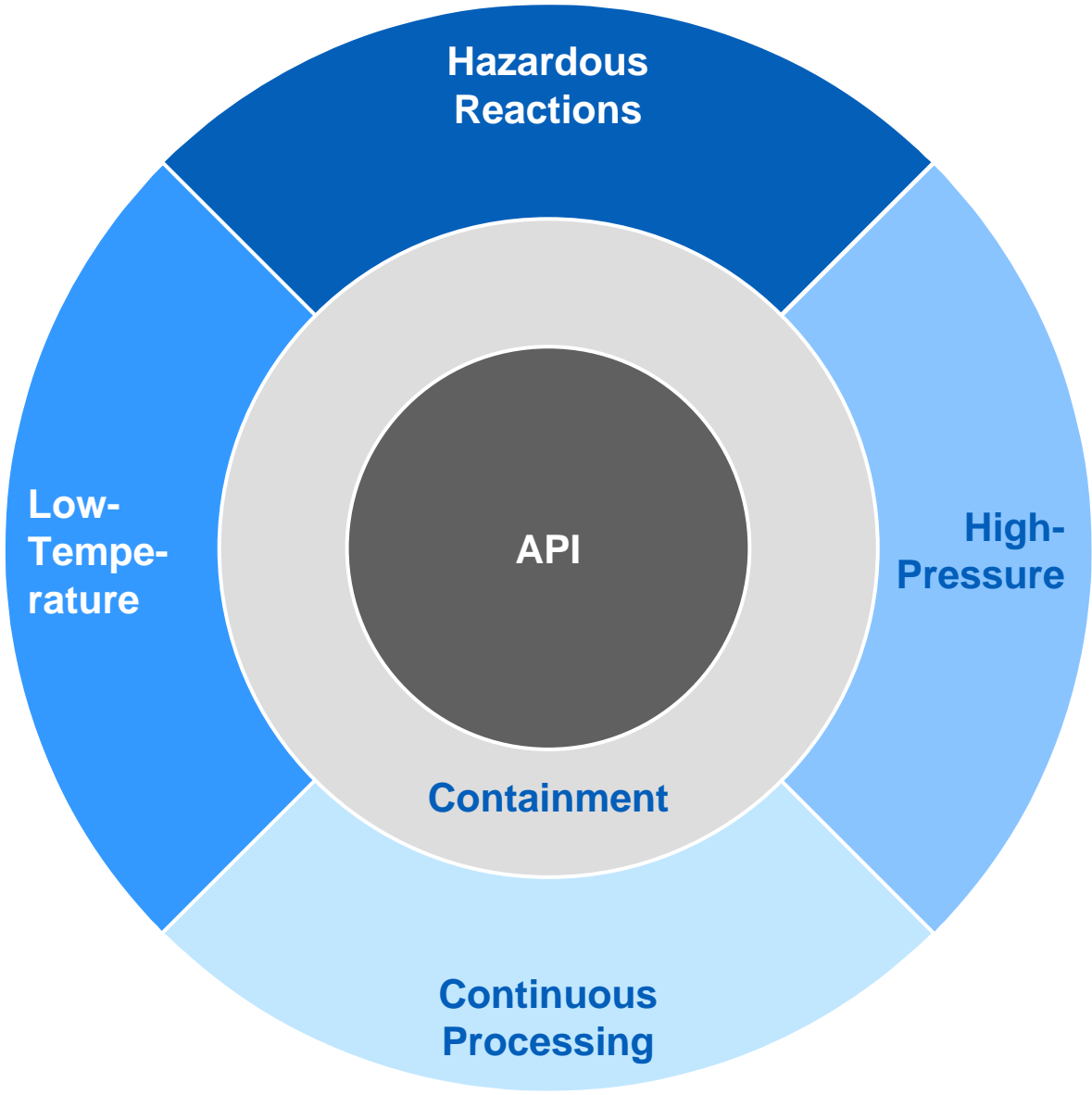
Case study I

Case study II

Summary

DOTTIKON EXCLUSIVE SYNTHESIS, Your Specialist for Hazardous Reactions.

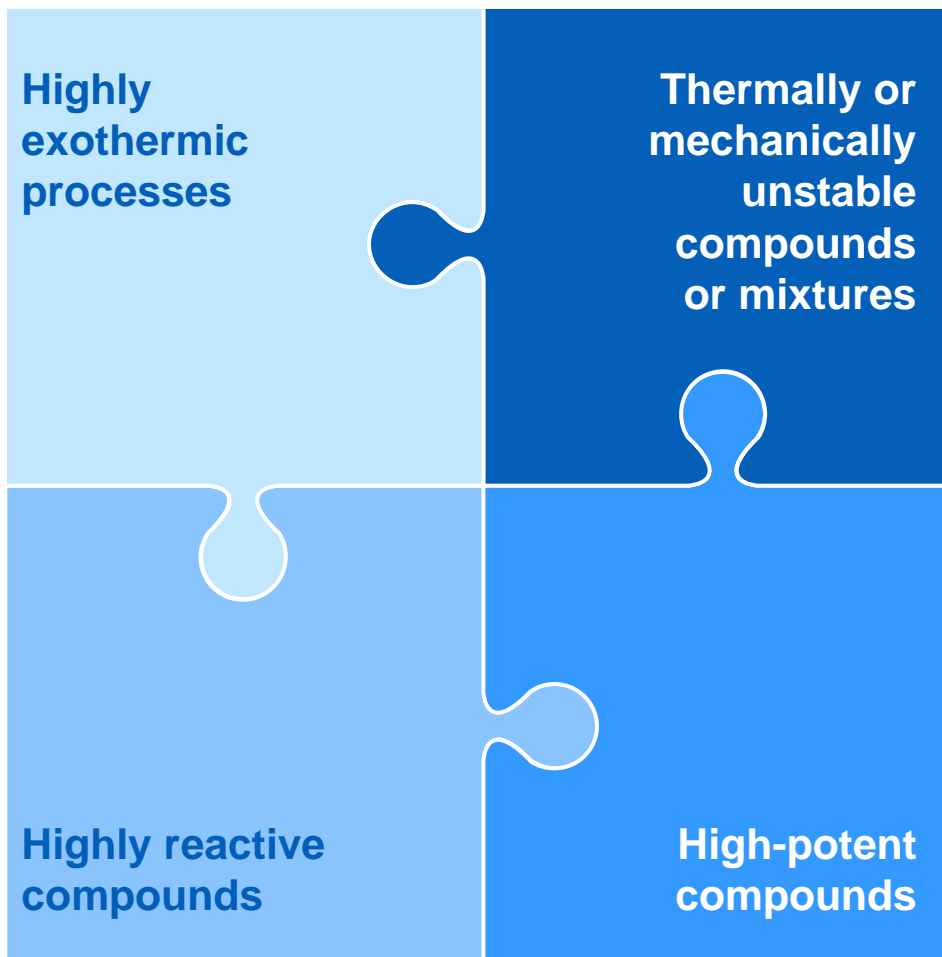






Hazardous Reactions

- Nitrations
- Grignard reactions
- Hydrogenations
- Oxidations



- Nitro compounds
- Azides
- Nitrate esters
- Peroxides
- Diazo compounds

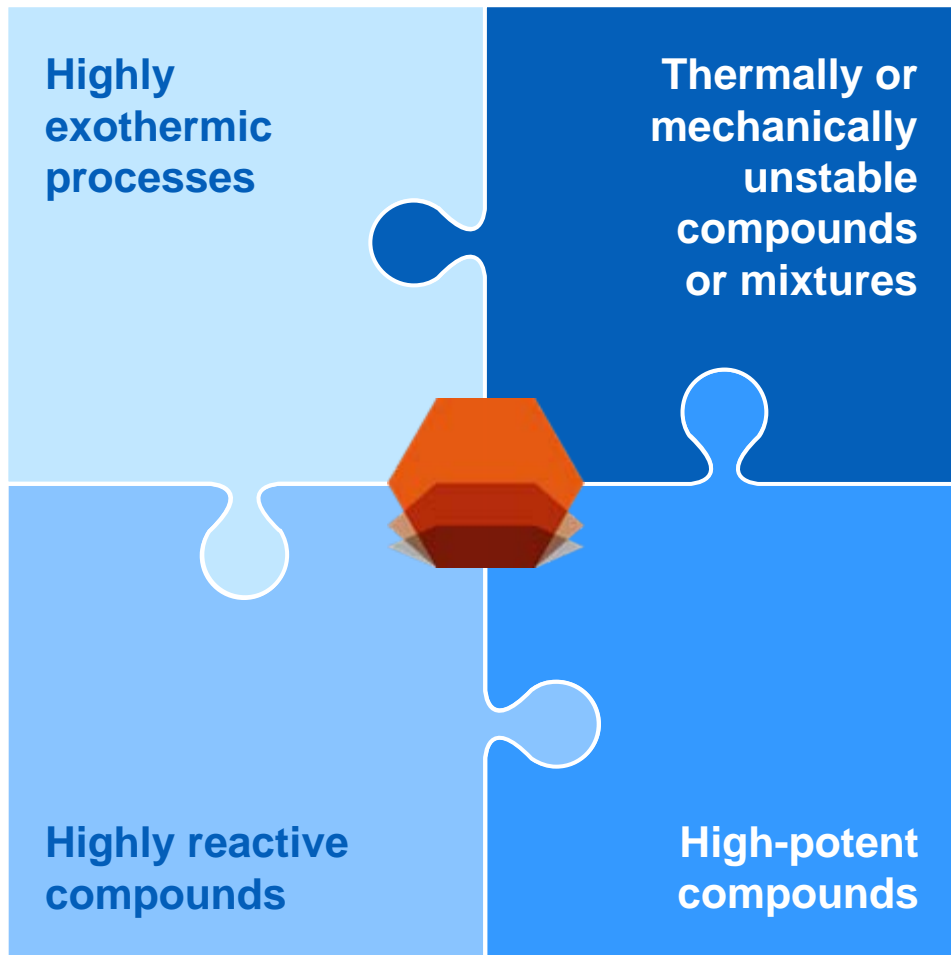
- Hydrides
- Dimethyl sulfate
- Nitric acid
- POCl_3 , PCl_5 ,
 POBr_3 , PBr_3
- SOCl_2 , SO_2Cl_2

- HAPIs
 - 20–100 $\mu\text{g}/\text{m}^3$
 - 1–20 $\mu\text{g}/\text{m}^3$
 - <1 $\mu\text{g}/\text{m}^3$



Hazardous Reactions at DOTTIKON ES

Prerequisites for Development and Production

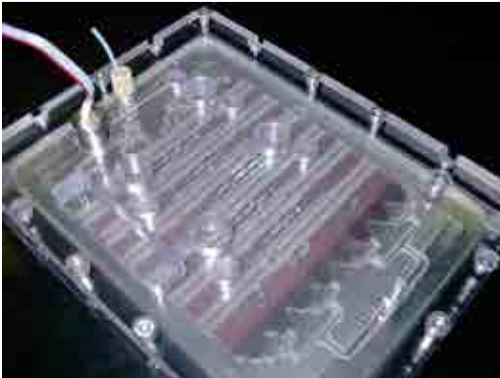


- Profound knowledge of critical process and engineering parameters
- Dedicated equipment on all scales
- Strongly developed safety culture

Over 40 Years of Experience in Continuous Processing



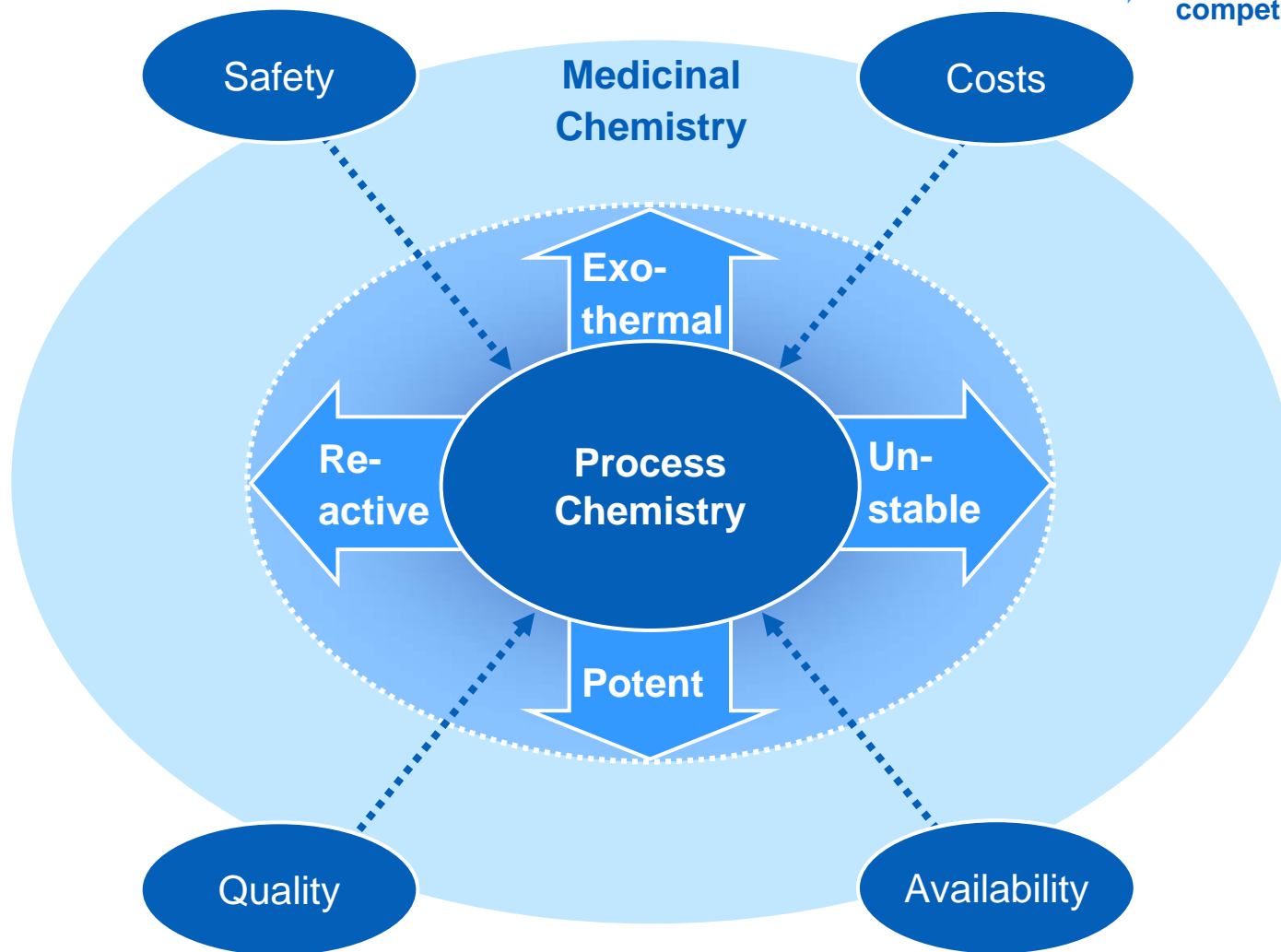
Micro reactors	Flow reactors	
	Kg's per hour	Multi-tons per hour





Competence in Innovative Technology Platform Allows Expanding Area of Reactions Choice

.....> Area-decreasing factors
➡ Area-increasing competencies



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Key Characteristics

Is continuous processing in pharmaceutical chemical production useful?

	Commodity products	Specialized products
Volumes	100's – 1'000's mt/year	1 – 100's mt/year
Demand	Steady	Variable
Quality	Standard quality	Customized
Production mode	Ongoing	Campaign wise
Plant type	Mono	Specialized multipurpose

Continuous

- High productivity
- Full automation
- High utilization

Batch wise

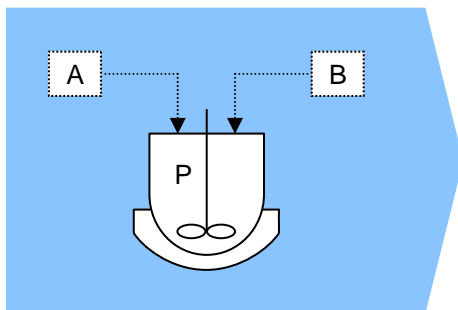
- High flexibility
- Semi automation
- Low product change effort



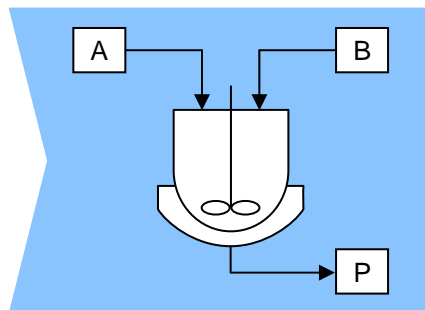
From Batch to Continuous

Different Reactor Concepts for Ideal Conditions

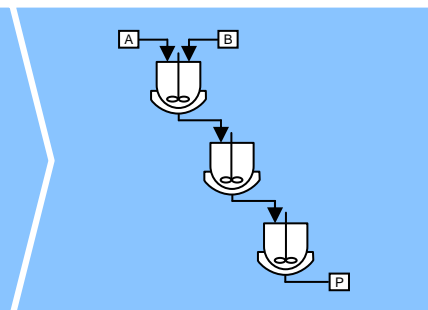
Batch



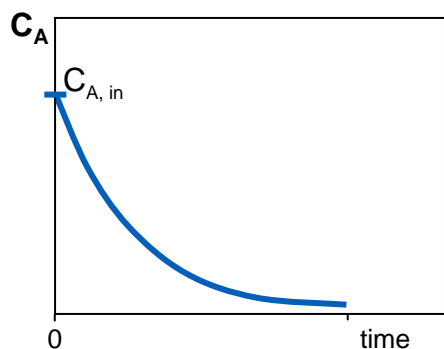
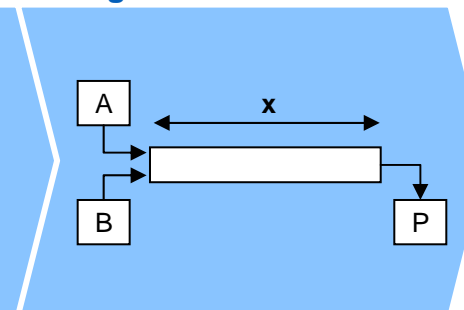
CSTR*



Cascade

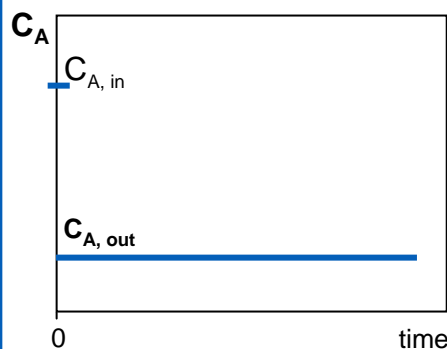


Plug Flow



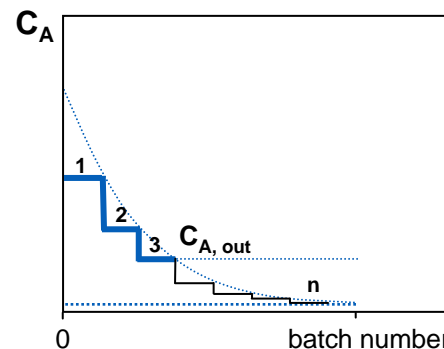
Composition change over time

- Suitable for most reactions
- Simple, flexible multipurpose equipment
- Batch
- Batch wise quality control
- High critical volume
- Low heat exchange capacity



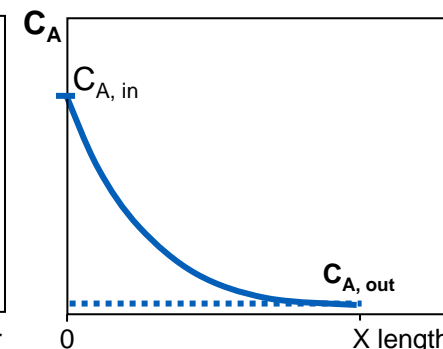
Composition constant over time

- Fast reactions
- Simple, flexible multipurpose equipment



Composition different, but constant in each reactor over time

- Fast and exothermic reactions
- Expensive and complex equipment



Composition change along reactor length

- Fast and exothermic reactions
- Inexpensive, dedicated equipment

- Online quality control
- Low critical volume
- High heat exchange capacity

* Continuous Stirred Tank Reactor

Comparison of Batch and Flow Reactor

Key Characteristics



	Batch reactor	Flow reactor
Basic requirements for reaction mixture	<ul style="list-style-type: none"> Homogeneous and heterogenous <ul style="list-style-type: none"> Solid Fluid Gaseous Up to high viscosity (stirrer power) 	<ul style="list-style-type: none"> Mainly homogeneous <ul style="list-style-type: none"> Fluid Gaseous Up to medium viscosity (pressure drops)
Adequate chemical reaction types	<ul style="list-style-type: none"> Most chemical reactions, however limited in the case of hazardous reactions 	<ul style="list-style-type: none"> Preferred fast kinetic Hazardous reactions <ul style="list-style-type: none"> Highly exothermic reactions Highly reactive compounds Toxic and high-potent compounds Unstable compounds (explosives) Kinetic controlled reactions (selectivity)
Scale-up and economics	<ul style="list-style-type: none"> Standard equipment from small to large scale with well-known characteristics 	<ul style="list-style-type: none"> Customized equipment engineered for specific throughput

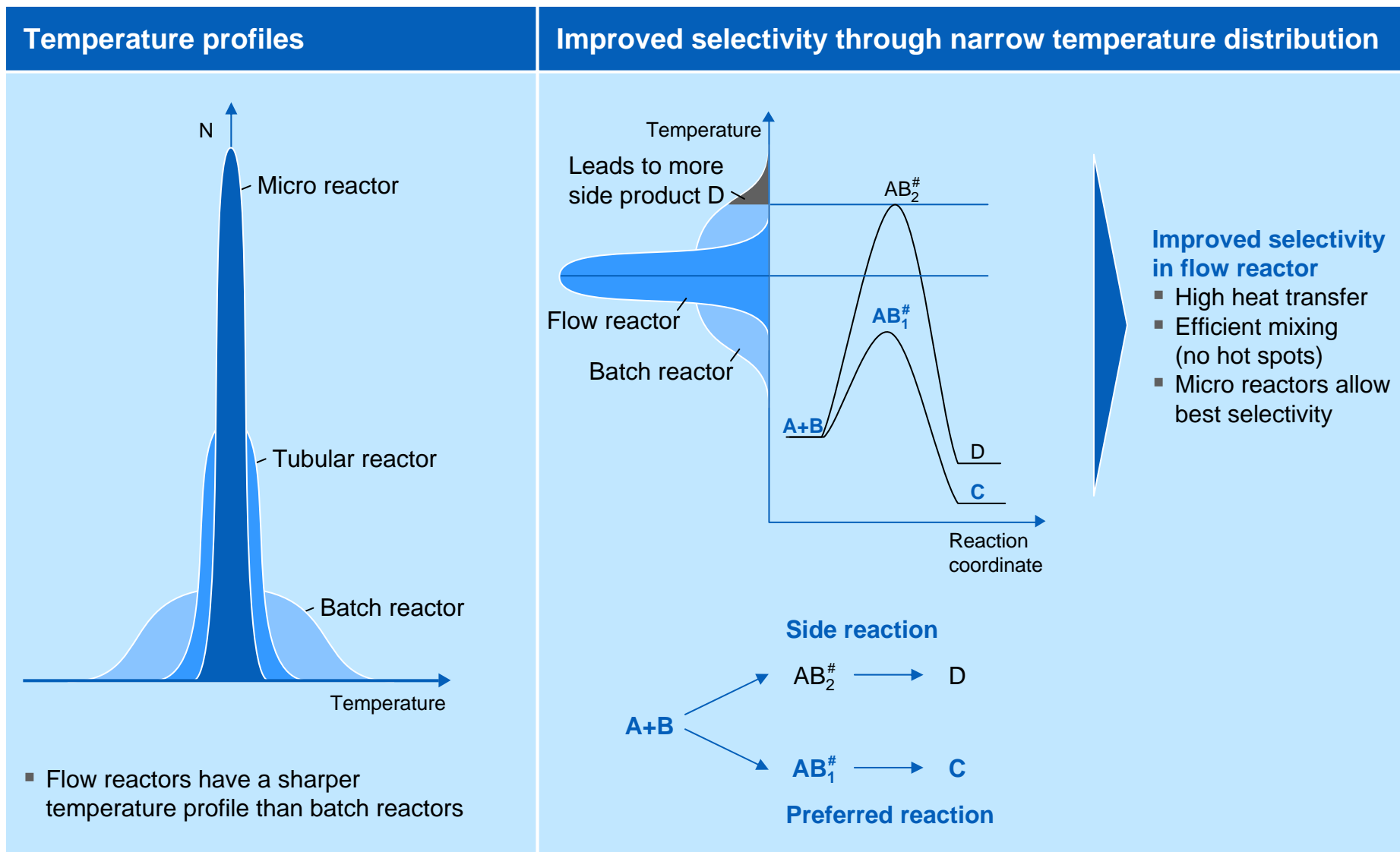
Continuous production for pharmaceuticals is useful whenever hazardous reactions are involved

Precise Temperature Profile Allows Kinetic Control

ILLUSTRATIVE

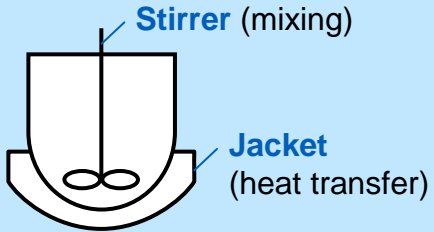
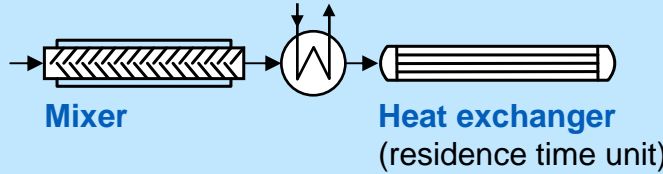
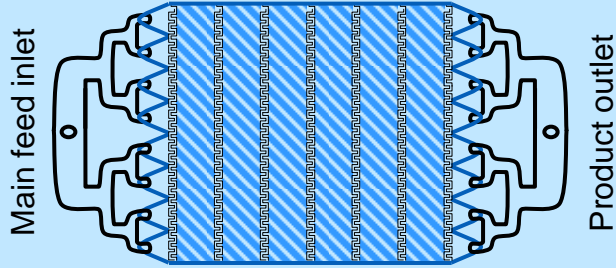

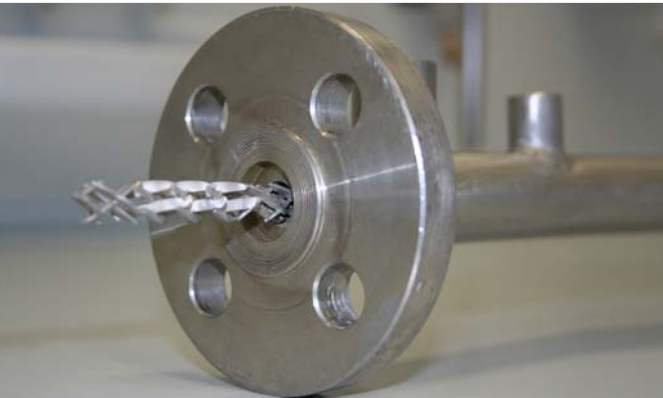
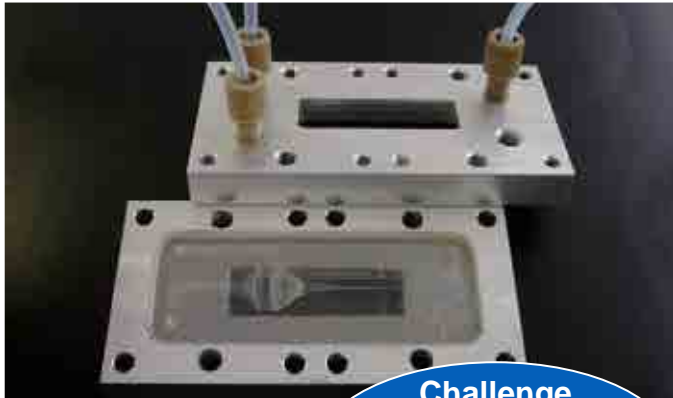


Reaction Selectivity



Engineering Parameters of Batch and Flow Reactors



Batch reactors	Flow reactors	
	Tubular reactor	Micro reactor
 <p>Stirrer (mixing)</p> <p>Jacket (heat transfer)</p>	 <p>Mixer</p> <p>Heat exchanger (residence time unit)</p>	 <p>Main feed inlet</p> <p>Product outlet</p> <p>Mixing/Reaction Zone</p>
		
<ul style="list-style-type: none"> ▪ Reactor volume <ul style="list-style-type: none"> ▪ $\text{dm}^3 - \text{m}^3$ ▪ Reactor geometry <ul style="list-style-type: none"> ▪ Spherical / Cylindrical ▪ Stirrer type ▪ Scale up 	<ul style="list-style-type: none"> ▪ Tube diameter <ul style="list-style-type: none"> ▪ $\text{mm} - \text{dm}$ ▪ Tube length ▪ Number of tubes and type of mixers ▪ Flow distribution system ▪ Scale up and parallelization 	<ul style="list-style-type: none"> ▪ Channel diameter <ul style="list-style-type: none"> ▪ $\mu\text{m} - \text{mm}$ ▪ Channel length ▪ Channel wall dimension and structure ▪ Flow distribution system ▪ Number of channels / numbering up

Challenge
Clogging of channels with insoluble side products

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Batch vs. Continuous

Development and Realization of Continuous Processes

Case study I

Case study II

Summary

Continuous Processing

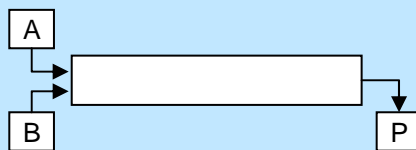
Chemistry

- Possible improvement of
 - Reaction rate
 - Selectivity
 - Yield
 - Quality
- Process intensification

Engineering

- Equipment fitted to chemistry
- High mass and heat transfer
 - Safety
 - Low critical volume
- Throughput
- Process control
- Automation

Continuous production



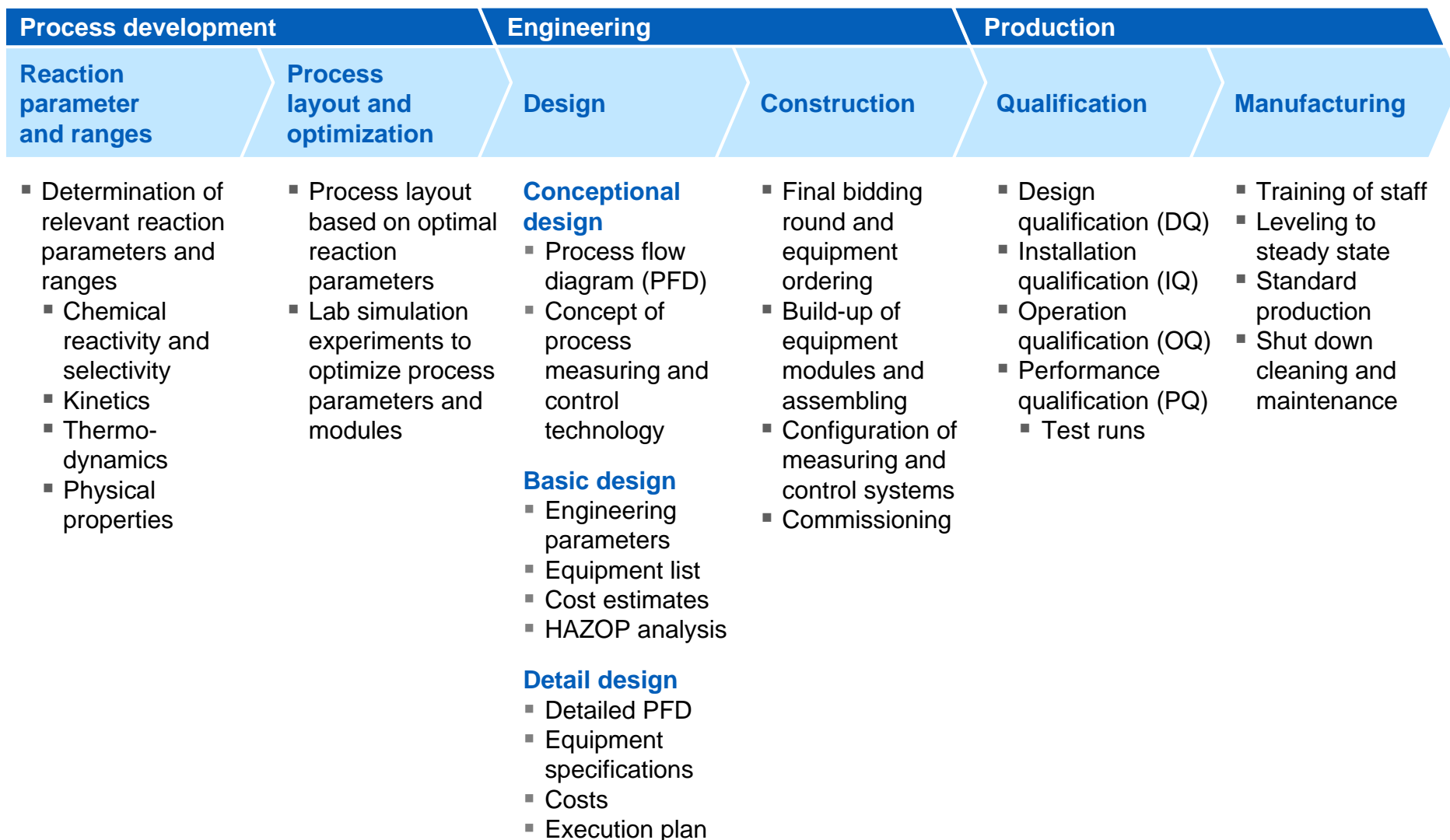
- Investment in dedicated continuous equipment

Economy

- Low production costs
 - High throughput/volumes
 - Automation
- High and constant product quality

Product

Development and Realization of Continuous Processes



Process Development of Continuous Processes

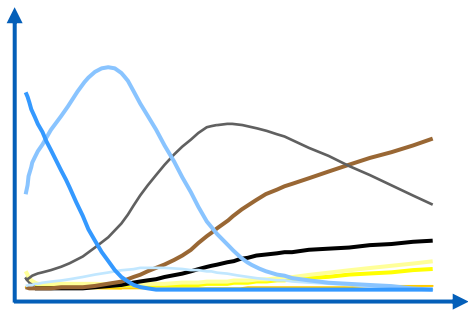


Determination of reaction parameters and ranges

One shot



Kinetics



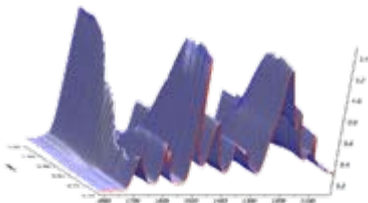
DSC



Reaction calorimetry



PAT



Process layout and optimization

Low-temperature CSTR



Micro reactor set up

Pumps

Cooling bath with microreaction unit, incl. reactor, residence time unit, quench, analytics

Feed solution

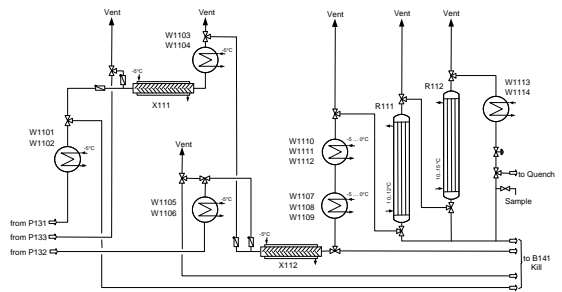
Product stream, analysis

Separating funnel

Engineering – Design and Construction of Continuous Plant



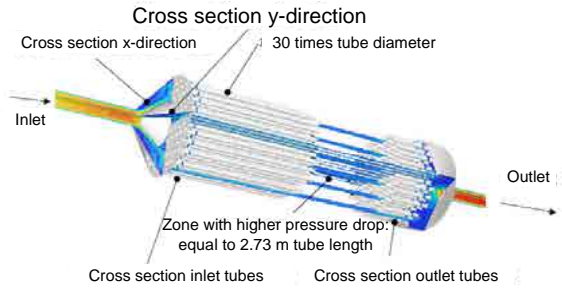
Conceptual



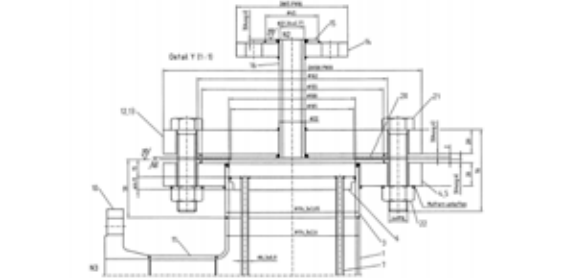
Construction and Commissioning



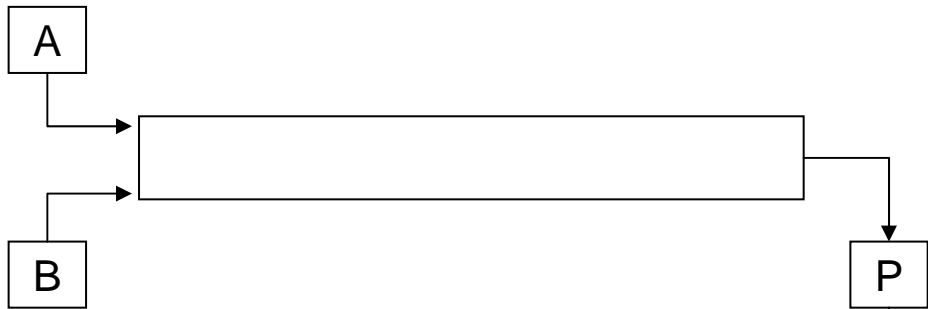
Basic



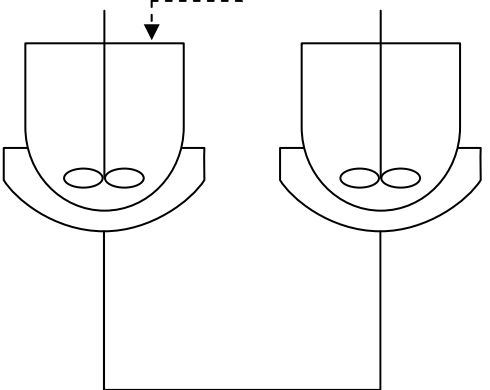
Detail



From Flow Reaction to Full Continuous Production



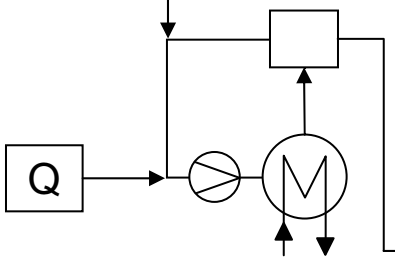
Batch quench and work up



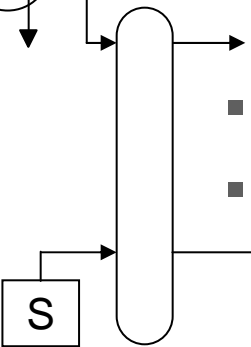
- Quench
- Extraction
- Distillation

Separation and Isolation

Continuous quench and work up



- Quench
- Extraction
- Distillation



Separation and Isolation

For long-term economic utilization, continuous processing to be extended to subsequent process steps

Introductionary Remarks to Continuous Process Case Studies

Case studies out of exclusive customer projects

- No disclosure of exclusive and proprietary know how
- No disclosure of process specific data

Case studies

- Two recent projects as examples for continuous processing
 - I. Know-how transfer from customer, engineering and fast realization (engineering, construction, installation, production) at DOTTIKON ES
 - II. Complete in-house process development/engineering/production of hazardous reaction

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Case study I

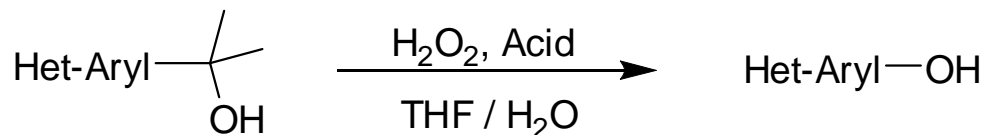
Case study II

Summary

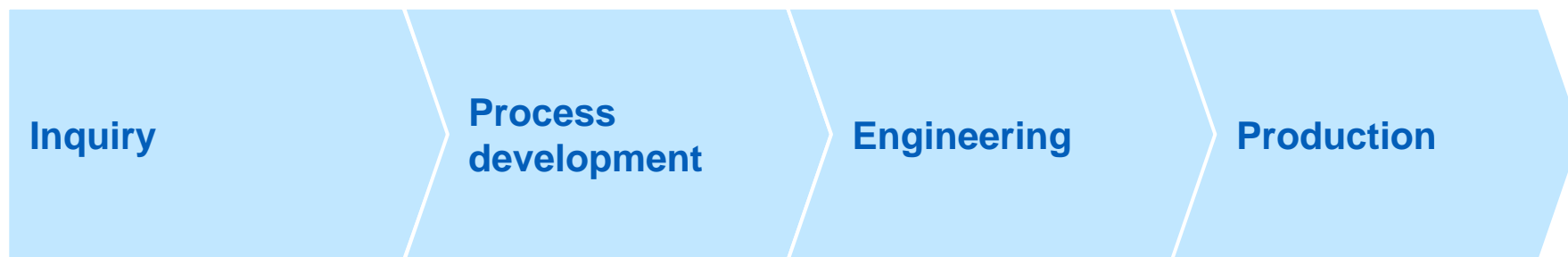
Case Study I – Control of Hazards by Continuous Processing



Oxidation using H₂O₂ (50%) as reagent and rearrangement



- Production of ca. 500–1'000 kg product as second step of a five step synthesis
- Continuous process developed by customer on lab scale (MRT) and small pilot scale
- Construction and installation of continuous equipment within 6 months
- All made in Hastelloy
- Design/engineering of new residence time unit

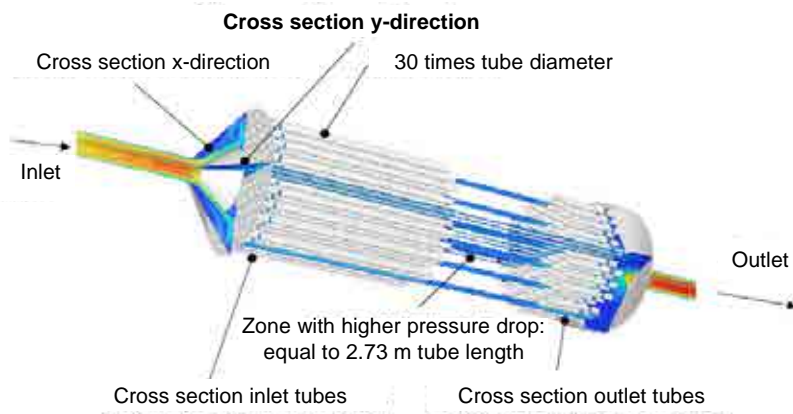


**From lab to production scale
in 6 months**

Case Study I – Design/Engineering of Residence Time Unit



Computed Flow Distribution Simulation

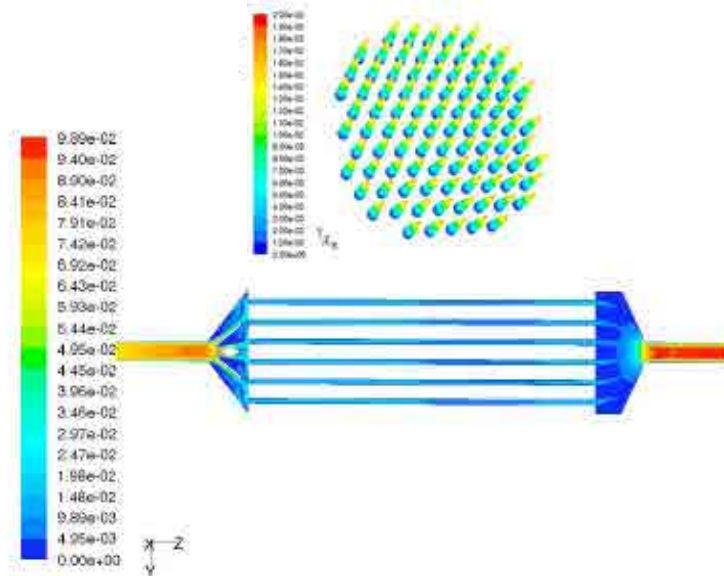


Targets

- Good flow distribution at the inlet for homogenous velocity
- No vortices (side products)
- Residence time of 12 minutes

Results

- Conical inlet with a special designed insert
- All requirements fulfilled



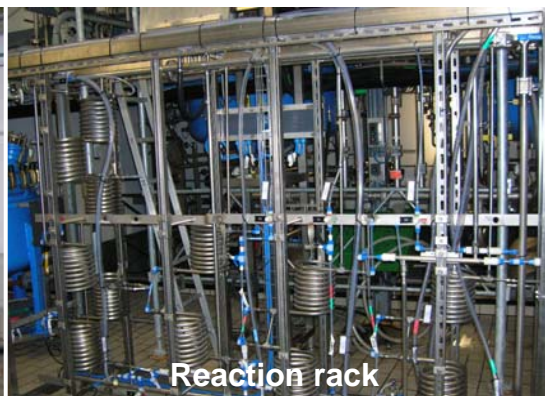
Case Study I – Production Equipment



- Batch wise quench and work up in plant (2 reactors in parallel, ca. 11 hour runs)
- Total flow: ca. 50 L/h
- Production of 500–1'000 kg isolated product per campaign



Feeding vessel



Reaction rack



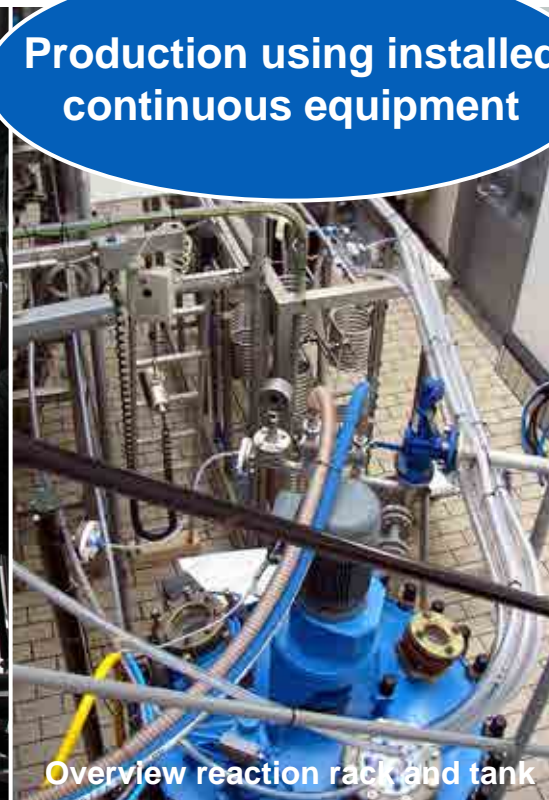
Pumps/flow meter



Cooling unit



Residence time unit



Overview reaction rack and tank

Production using installed continuous equipment

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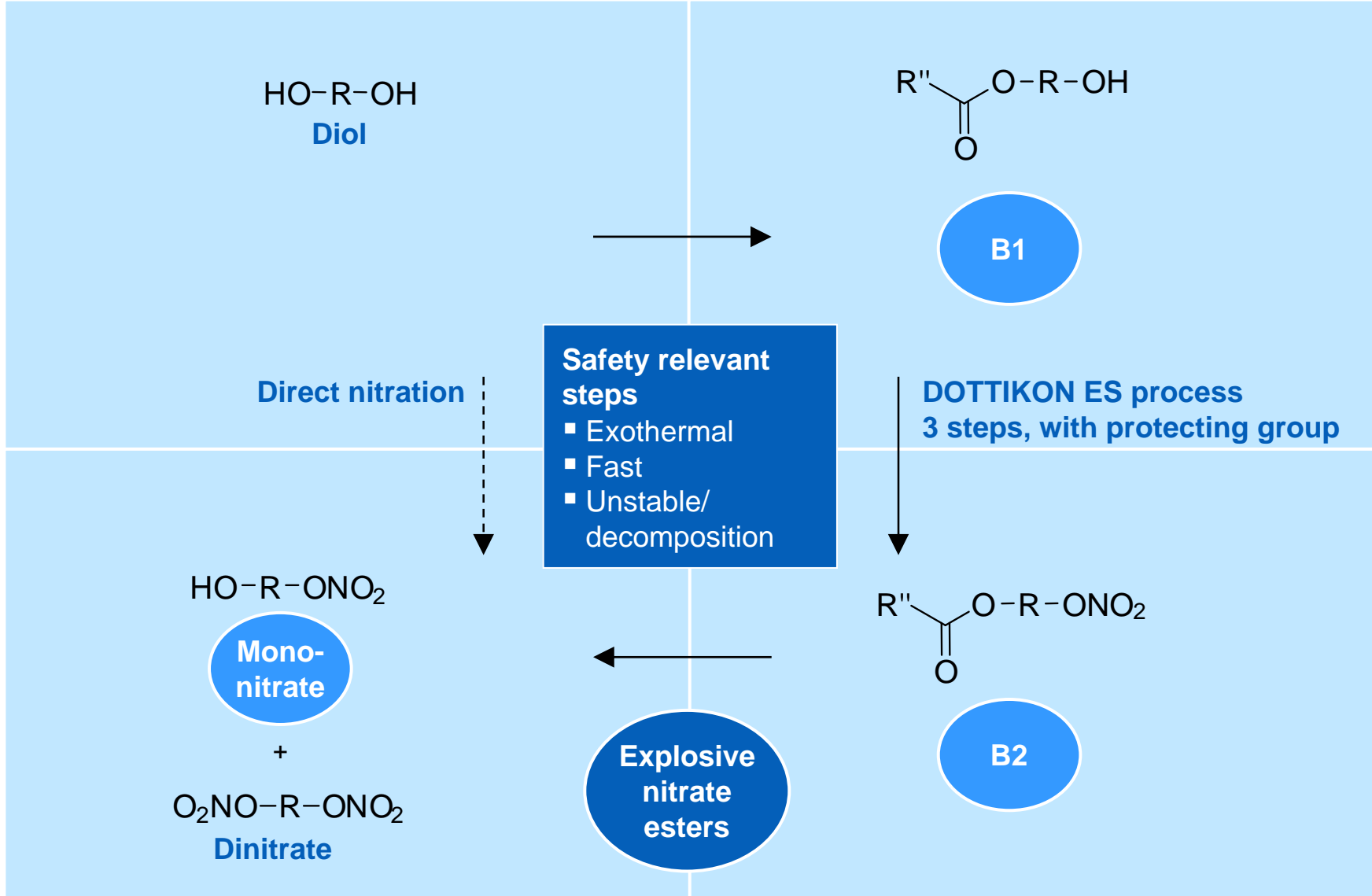
Development and Realization of Continuous Processes

Case study I

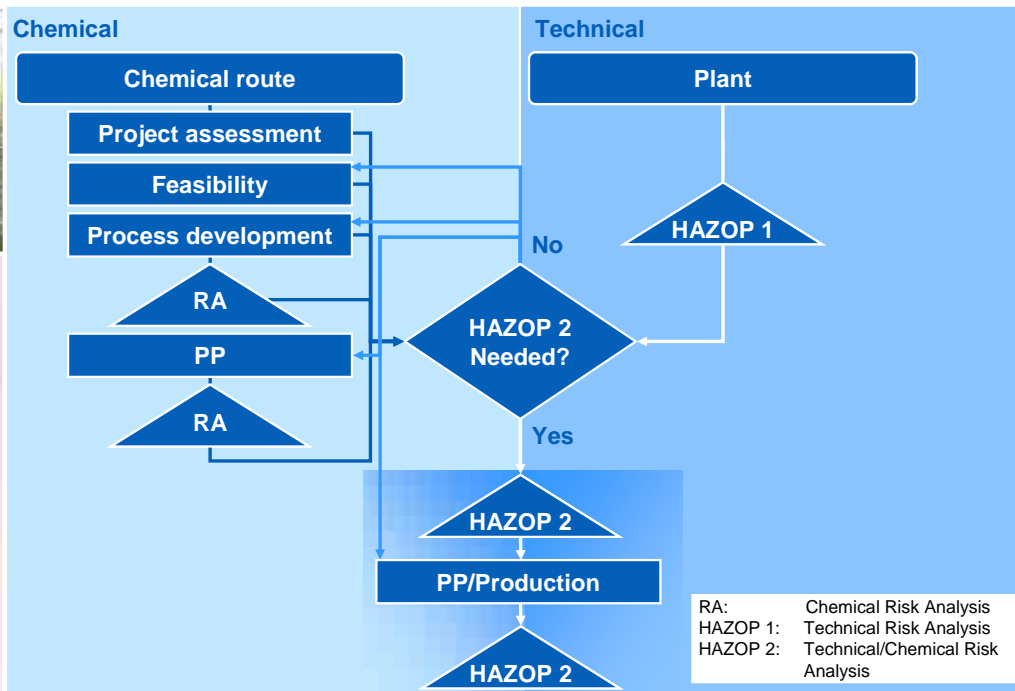
Case study II

Summary

Case Study II – Production of Mononitrate



Case Study II – Risk Analysis and HAZOP



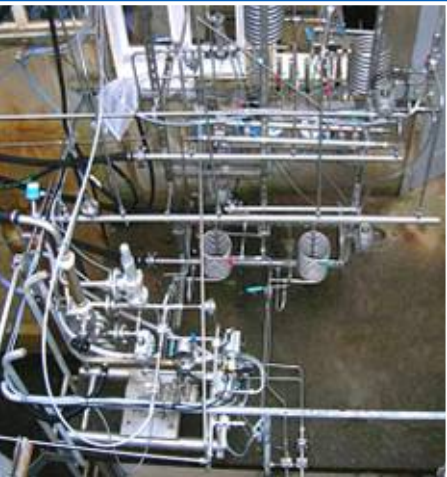
Case Study II – Production



Feed tanks



Tubular reactor unit



Quench unit

Control units



Cooling unit

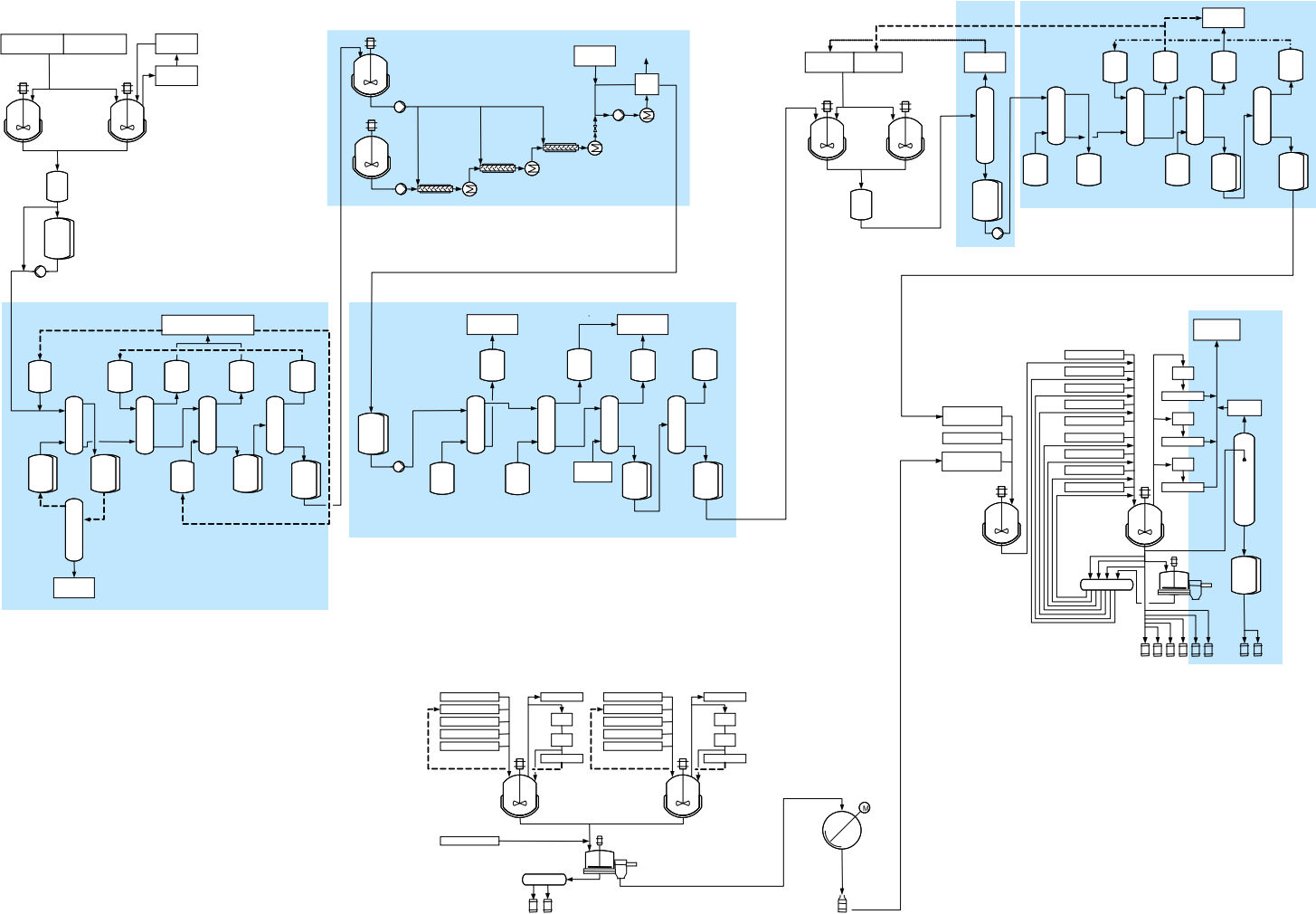
Continuous extraction unit



Case Study II – Investment Phases for Scale-up



Continuous unit operation



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Summary and Conclusion

Summary

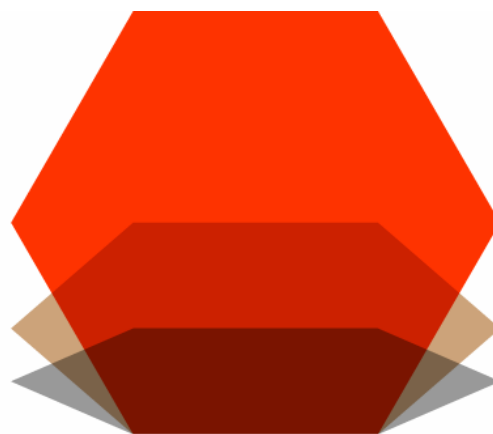
- Continuous processing in pharmaceutical chemical production is useful when reactions have
 - Fast kinetics
 - Hazardous chemistry involved
 - Selectivity issues
- Engineer flow reactors always as small as needed, but never as small as possible
- In scale-up, volume increase (size) outnumbers equipment multiplication (number) economically

DOTTIKON ES, your partner in continuous processing

- Process development
- Engineering and manufacturing
- Process transfers and scale-up

DOTTIKON's Continuous Specialists





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EXCLUSIVE
SYNTHESIS

Your Specialist for Hazardous Reactions.