

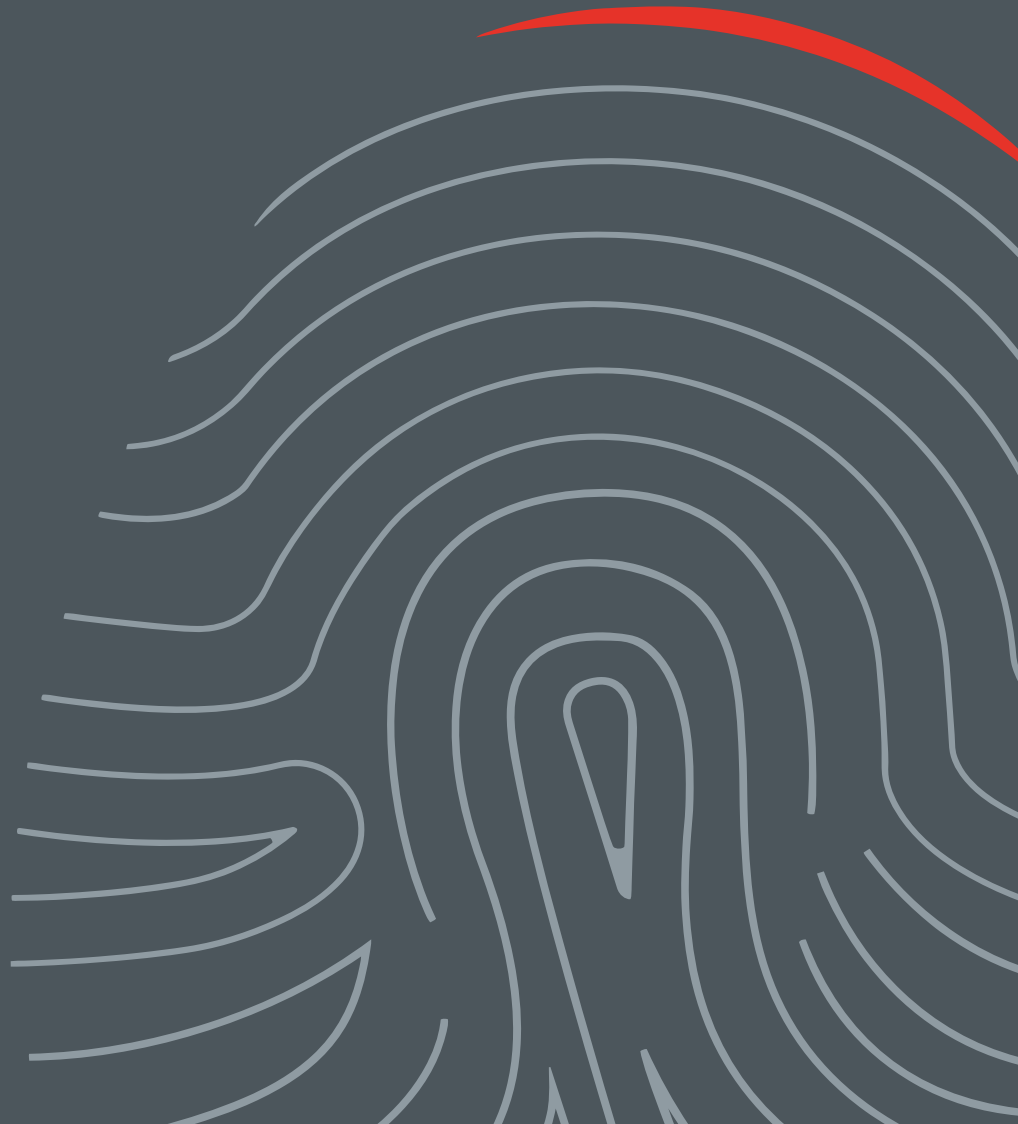


**Biocatalysis and  
bioprocessing -**

**Genes to GMP**

*Prof. Tom Moody*

[www.almacgroup.com](http://www.almacgroup.com)



# <sup>2</sup> Bioprocessing



**An integrated group of biologists and chemists who:**

**Discover.** New enzyme discovery platforms

**Screen.** Screen for and utilize enzymes in processes

**Evolve.** Improve properties of enzymes (process efficiency, economics)

**Supply.** Manufacture (immobilised) enzymes and enzyme-derived products



## **Key Expertise:**

- Enzyme discovery (metagenomics)
- Building panels of enzymes
- Active site modelling and enzyme design
- Evolution tools (saturation mutagenesis, random mutagenesis)
- Fermentation development & scale-up
- Enzyme immobilization & supply
- Bioprocess development and manufacture of chemicals
- Metabolite synthesis

# 3 Reaction Experience



Decades of process experience....

Reaction Experience		
Alkylation	Enzyme immobilisation	Nitrilase reactions
Aminoalkylation	Heck Reaction	Optical Resolution
Asymmetric Synthesis	Hydrogenation	Organolithium Chemistry
Biotransformations	Hydrolase bioreolutions	Organometallics
Base Catalysis	Grignard Reactions	Organosilicon Chemistry
Transfer Hydrogenation	KRED bioreductions	Oxidation
Condensations	Reductions	P450 Biooxidation
Dealkylation	Leuckart Reaction	Ritter Reaction
Dieckmann Condensation	Methylations	Stereoselective Reactions
Diels Alder Reaction	Michael Reaction	Suspension polymerisation
Enzymatic Resolution	Mannich Reaction	Transaminase bioreactions

...Coupled with biocatalysis manufacturing technologies

# 4 Manufacturing



**Ideal tank sizes to develop and manufacture Multi-Ton scale intermediates (biocatalytic processes & immobilisation)**

## **Multi-purpose Pilot Plant**

- 7 reactors from 100 to 1,000L
- Total capacity of 2,600L
- Glass-lined, Hastelloy and Stainless Steel



## **Manufacturing Plant**

- 13 reactors from 2,200L to 6,300L
- Total capacity of 45m<sup>3</sup>
- Glass-lined and Stainless Steel



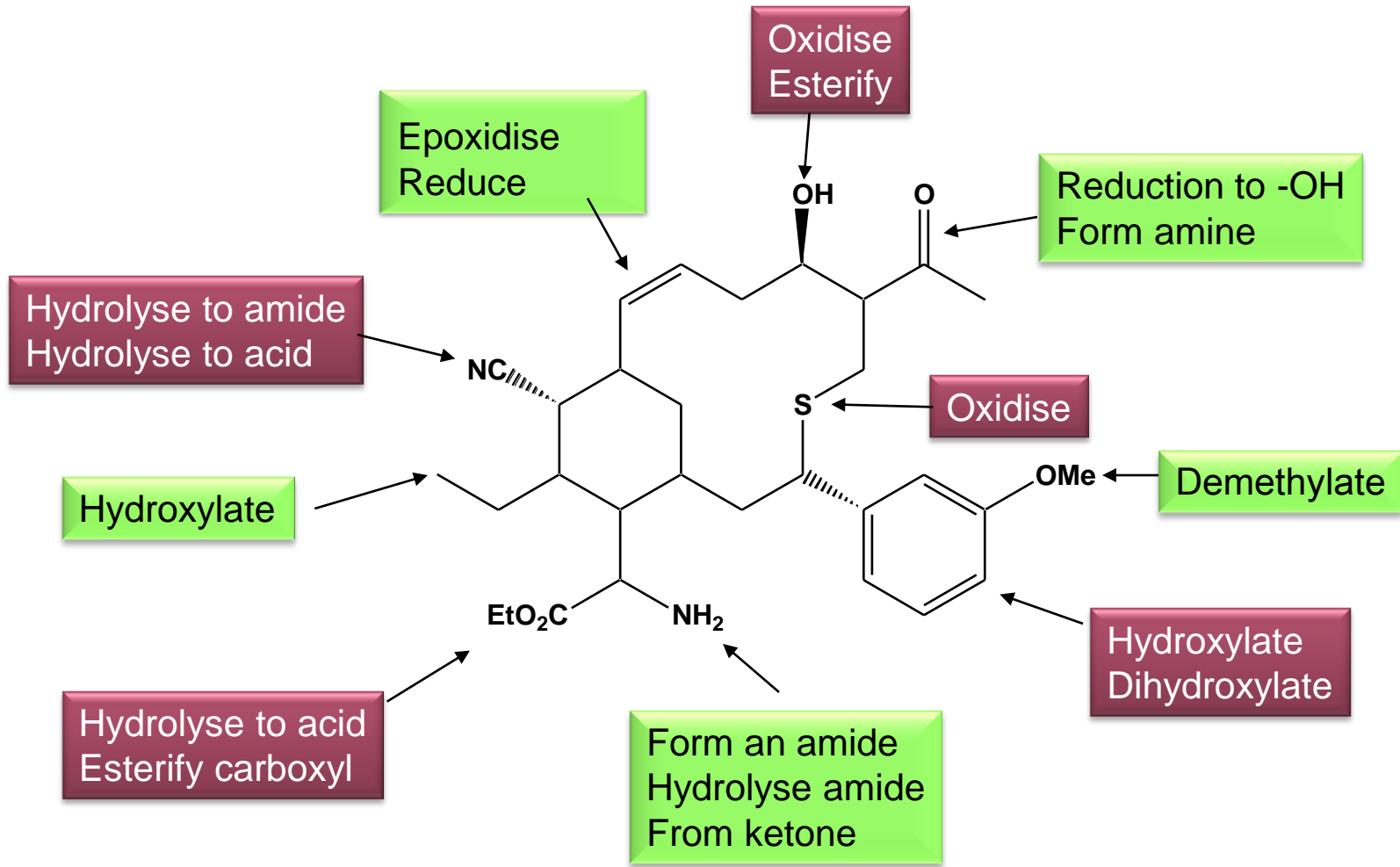
## **Work-up**

- Centrifugation from 1.0 to 2.5 tonne
- Driers: 0.5 to 0.6 tonne



**arran**  
CHEMICAL COMPANY LTD  
A Member of the Almac Group

# Almac Technology



# 6 Almac Technology



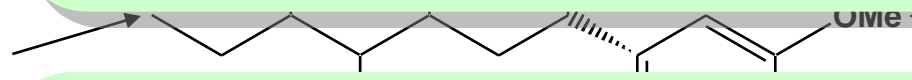
### The Good Bits

- ✓ Chemo & Regioselective
- ✓ High stereoselectivity
- ✓ Simple and easy to perform

Hydrolyse to amide  
Hydrolyse to acid

Conversion to -OH  
amine

Hydroxylate



Demethylate

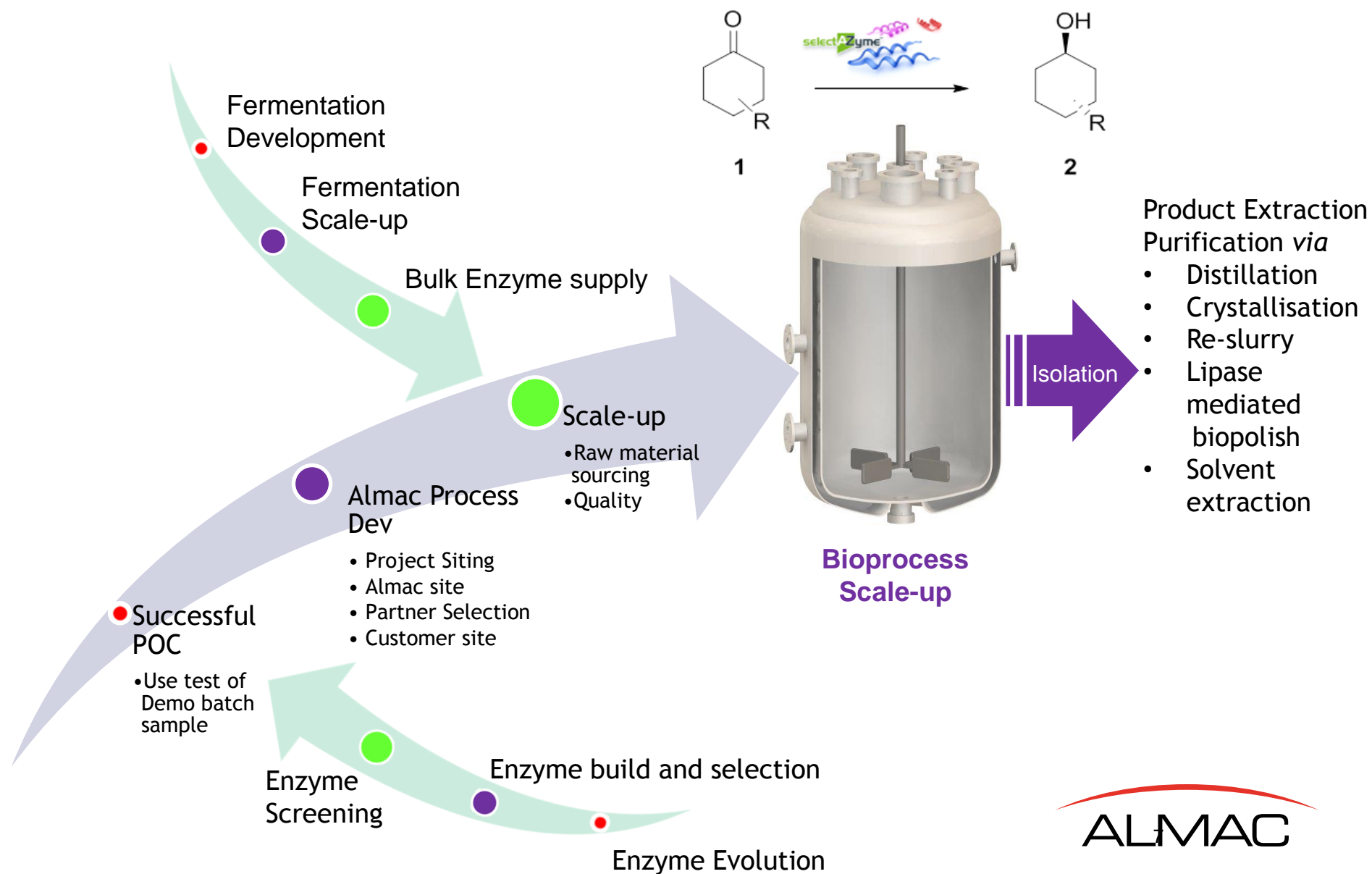
### Green & Sustainable

- ✓ Water as the solvent
- ✓ Ambient temperature
- ✓ Atmospheric oxidant
- ✓ Non toxic waste

Hydrolyse to acid  
Esterify carbonyl

Hydroxylate  
hydroxylate

# kg to tonne manufacture





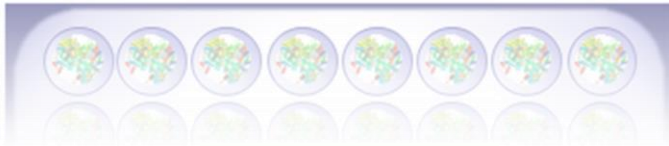
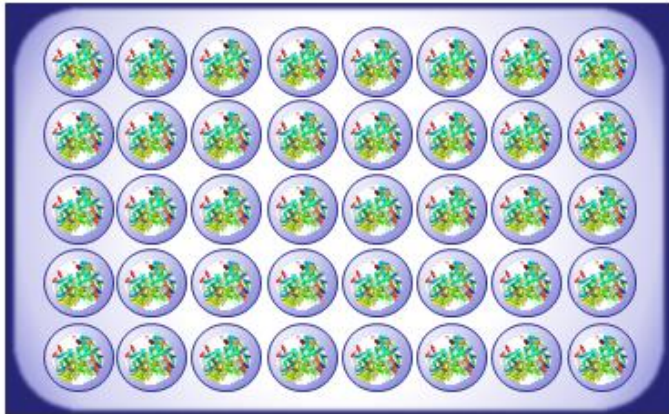
# Specific Enzyme Panel Building



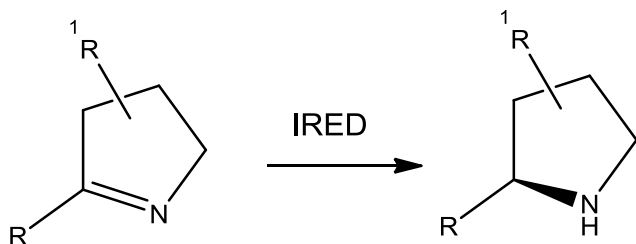
# 9 Enzyme panel building



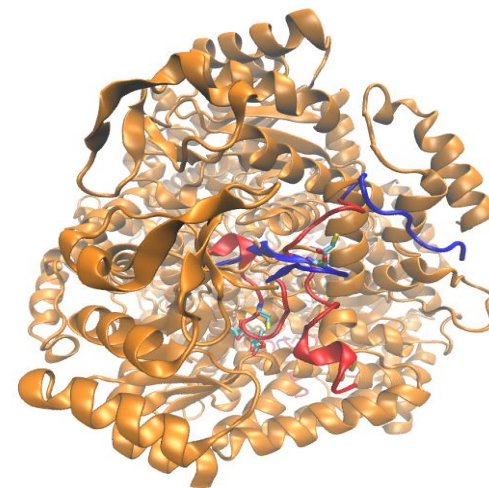
## Bespoke enzyme panel



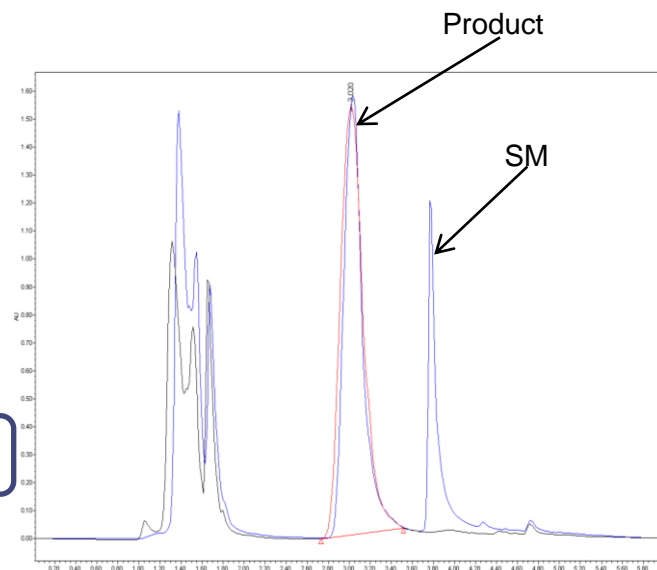
- Bespoke enzyme panels can be developed within weeks using Almac bioinformatics GIDS platform
  - GIDS – gene informed database searching
  - Tailormade panel of enzymes expressed in 96 well plate format
- 
- 1 enzyme only possible; typical is 25, 50 or 96
  - 1g to tonne supply of enzyme available



- *In silico* design of 50 IRED enzyme library
- Gene synthesised, cloned and expressed
- Screened against customer substrate – hits found



IRED no.	% HPLC peak area @ 260 nm		% HPLC peak area of product enantiomers		ee
	Product	SM	(S)	(R)	
3	9	91	54	46	8
5	2	98	0	100	100
8	77	23	89	11	78
9	2	98	13	87	74
12	3	97	100	0	100
16	3	97	77	23	54
20	100	0	100	0	100
26	1	99	89	11	78
27	31	69	92	8	84
28	8	92	0	100	100



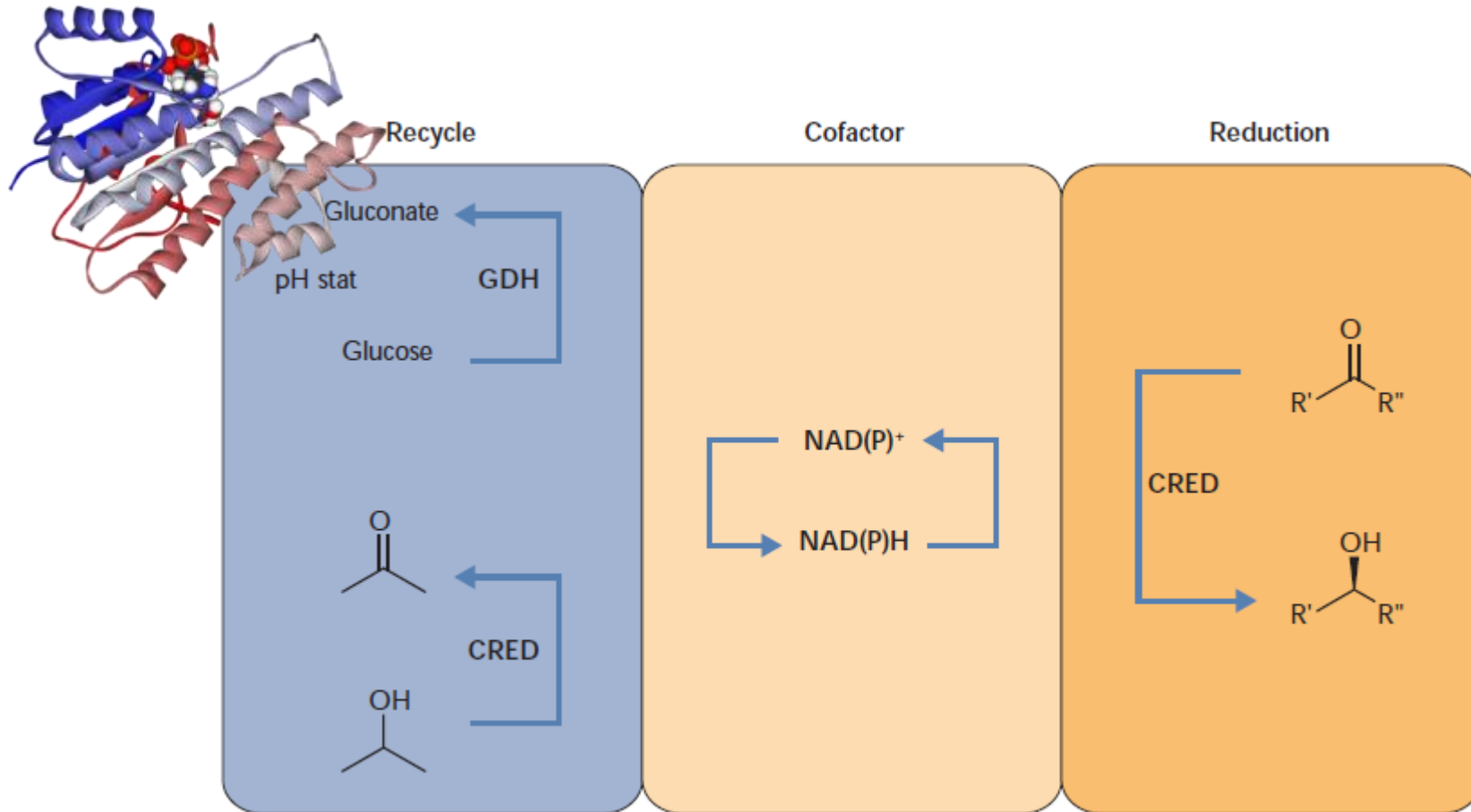


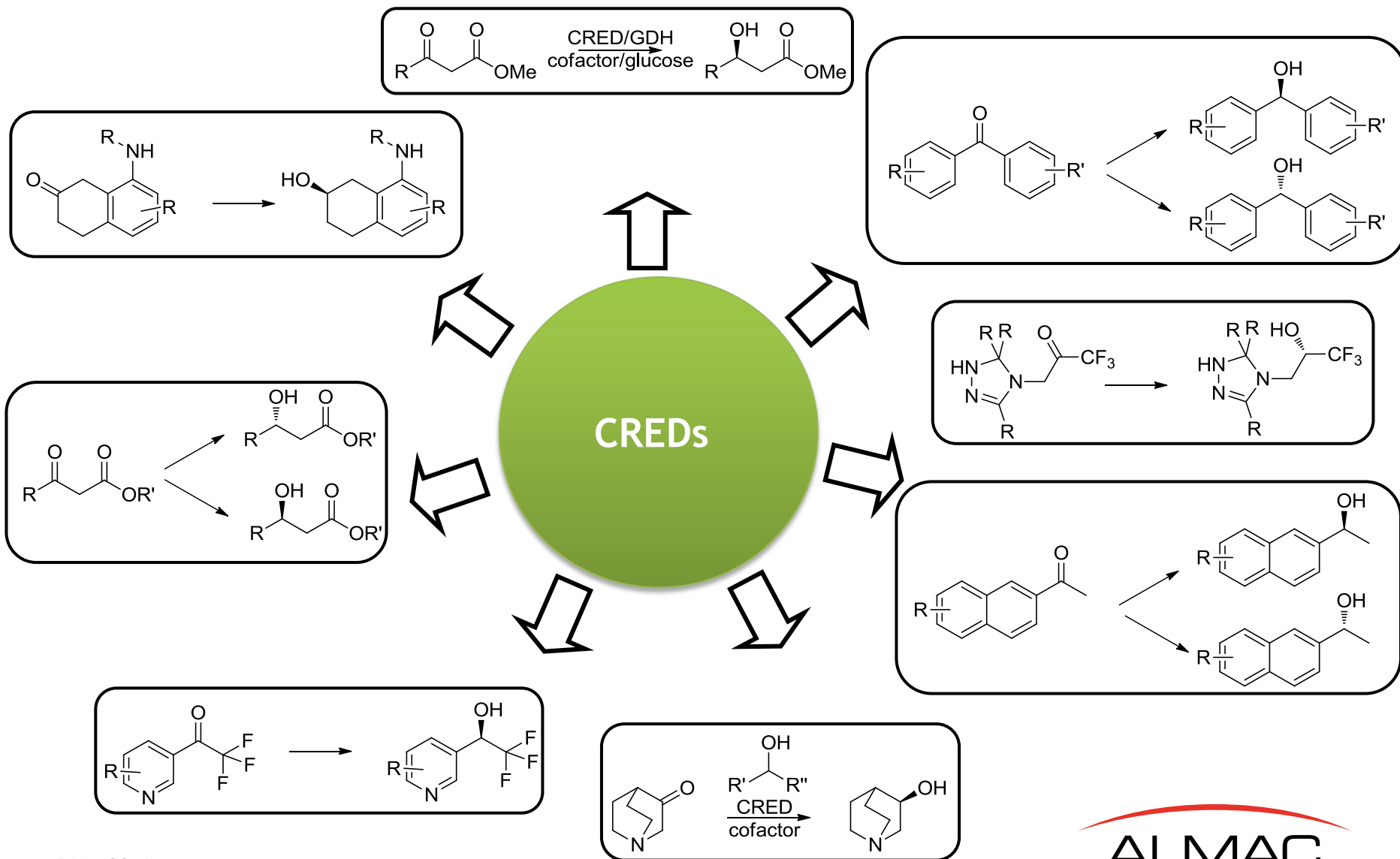
# CRED enzymes

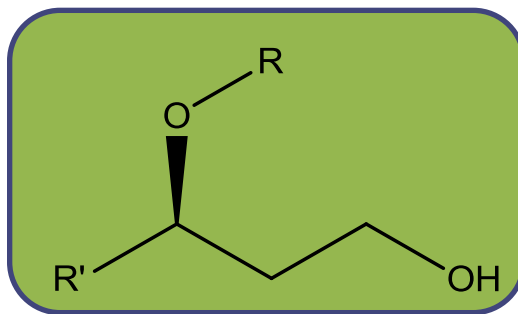
# CREDS



## Reaction mechanism



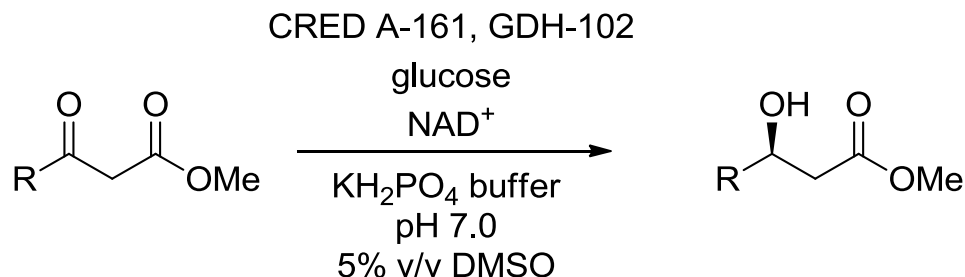




Chemocatalysis failed to deliver new specification of >99.2% ee

- Project for a Japanese Customer
- Building block for Phase III API
- Specification: >99% (GC), max. 0.1% for unknown imps, up to 0.5% named imps; >99% ee
- No scaleable biosynthetic route to intermediate
- Fermentation scale-up to 1000s of litres
- Ultimately tonne process required
- <<\$1000 / kg

# Bioreduction



## CRED Screening:

- A161 identified as hit with >99.5% ee
- Enzyme is NADH-dependent
- GDH/glucose used for co-factor recycle

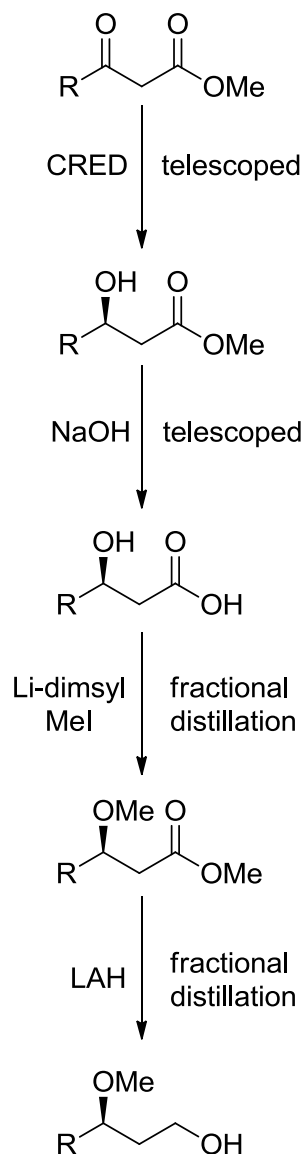
## Process Optimisation:

- 5% DMSO co-solvent, pH 7.0, 30 deg C
- 0.1% w/w of lyo cell free extract CRED/GDH sufficient
- 180 g/L substrate >99.8% converted within 12 hours
- Workup by extraction with MtBE; crude product telescoped into next step

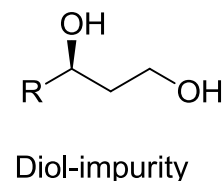
# Bioreduction



## Impurity control

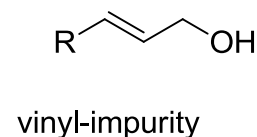


*Control of Diol-impurity starts here.*  
High reaction completion target  
of > 99.8% conversion.



*Control of alk-3-enol impurity starts here.*

High reaction completion targets.  
Choice of base for deprotonation.  
Unstabilised THF used for methylation.  
Fractional distillation in both final steps.



**Achieved:**  
99.3% ee; diol <0.2%; alk-2-enol <0.15%  
BHT and Me-BHT <0.2%, all other <0.1%



# Bioreduction



*from POC sample to commercial output*

**5 Step Process Yields**  
(%POC / %pilot batch / %final)

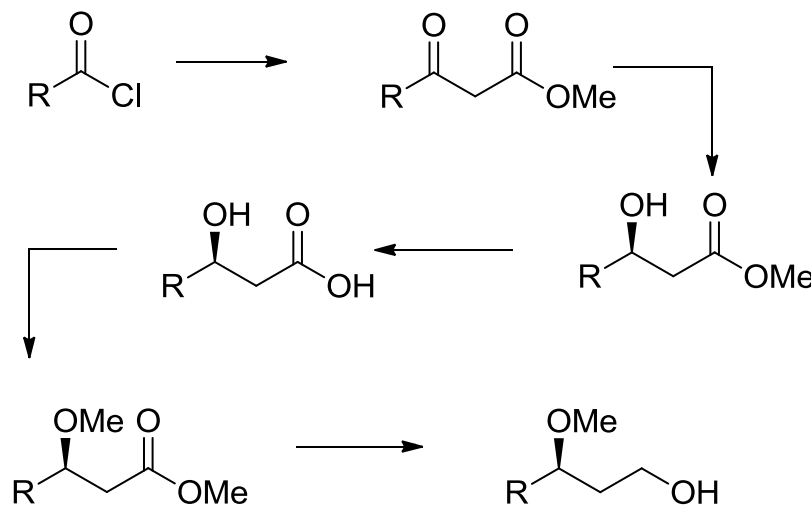
Step 1: 75% / 50% / 85%

Step 2: 91% / 90% / 95%

Step 3: 95% / 95% / 98%

Step 4: 80% / 70% / 85%

Step 5: 70% / 70% / 75%



*Process modifications after pilot batch experience:*

Step 1: switched from Meldrum's acid to methyl potassium malonate SM

Step 4: switched from n-BuLi to n-HexLi, relaxed specification

Step 5: improved hydrolysis protocol



# ERED enzymes

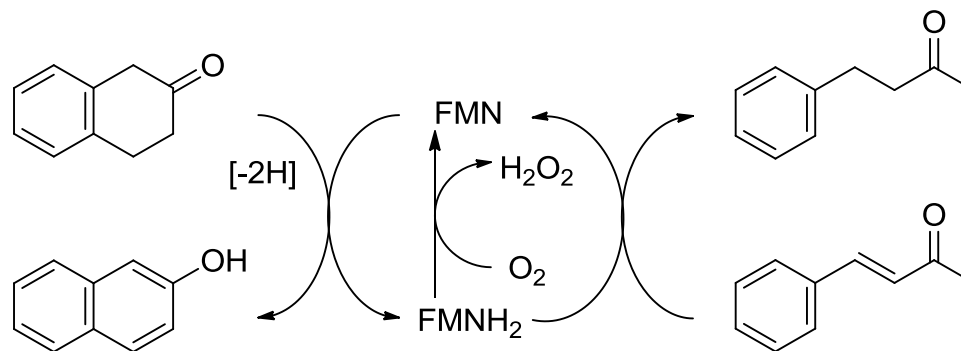


# Aromatisation Using Ene Reductase Enzymes

Paul P. Kelly<sup>a\*</sup>, David Lipscomb<sup>a</sup>, Derek J. Quinn<sup>a</sup>, Ken Lemon<sup>a</sup>, Jill Caswell<sup>a</sup>, Jenny Spratt<sup>a</sup>, Birgit Kosjek<sup>b</sup>, Matthew Truppo<sup>b</sup> and Thomas S. Moody<sup>a</sup>

<sup>a</sup>Almac, Department of Biocatalysis Isotope Chemistry, 20 Seagoe Industrial Estate, Craigavon, BT63 5QD, Northern Ireland, United Kingdom, Phone: +44 (0) 28 3833 2200; e-mail: [paul.kelly@almacgroup.com](mailto:paul.kelly@almacgroup.com)

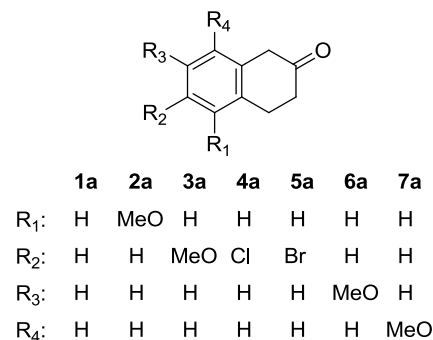
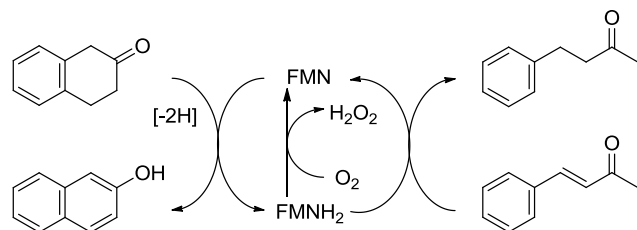
<sup>b</sup>Merck & Co., Inc., Department of Process Research, Merck Research Laboratories, P.O. Box 2000, Rahway, New Jersey 07065, USA



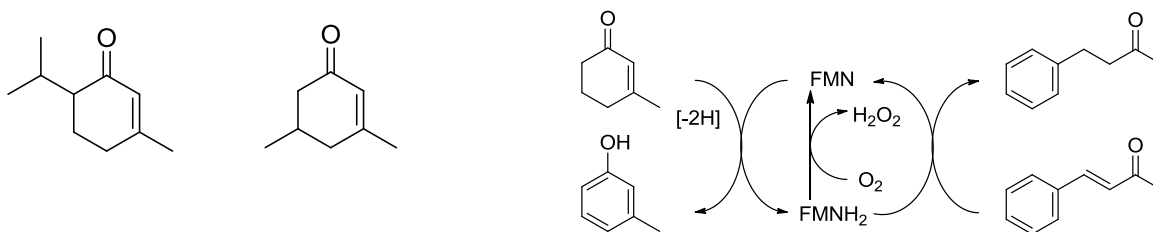


## EREDs for Phenol/Naphthols (*Adv. Synth. Catal.*)

- Conversions of tetralones to naphthols in absence of reduction target (**9a**) confirmed up to >99% in some cases



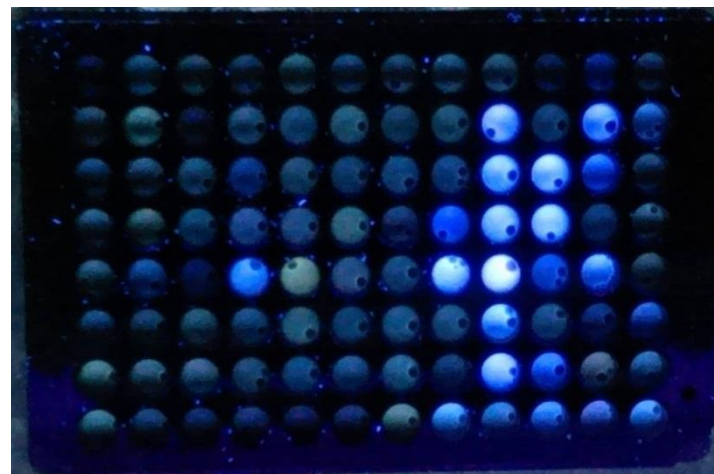
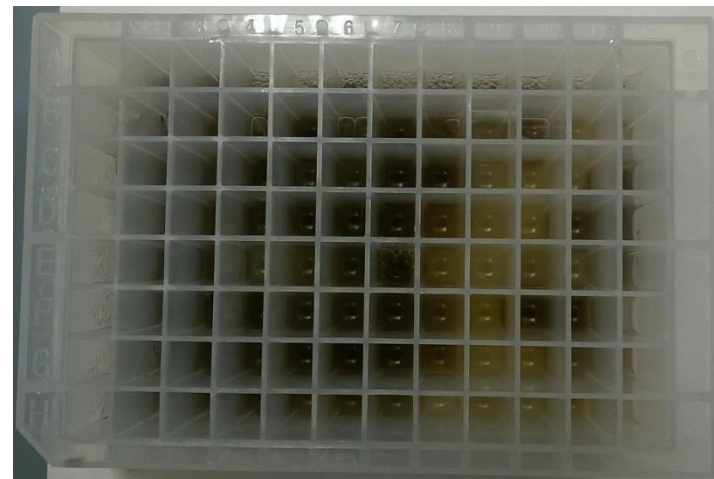
- ERED 69 and 7-MeO-Tetralone selected for optimisation and scale up to ~1g to follow
- Additional examples of cyclohexenones to phenols to be included





## Analysis by Fluorescence

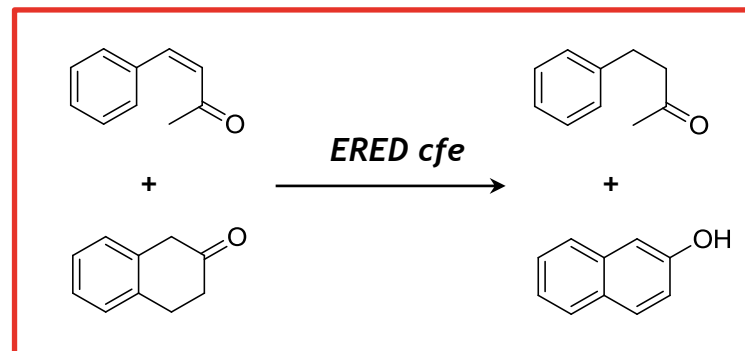
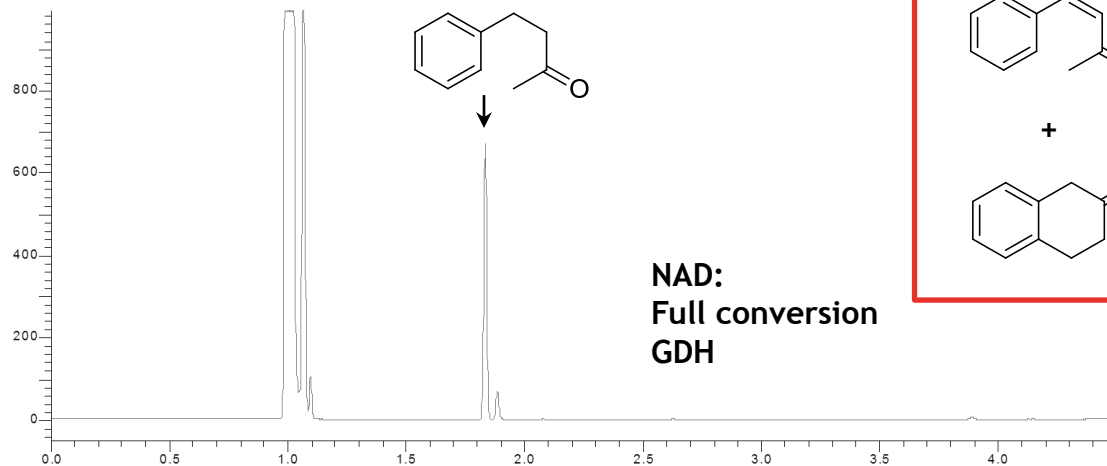
- Red-orange precipitate in many wells
- Others clear/yellow
  
- 200  $\mu$ l of sample taken
- 22  $\mu$ l of 1M NaOH added
- Observed under UV (365nm)
- Read by fluorescence plate reader
  - $\lambda_{ex}$  = 355 nm,  $\lambda_{em}$  = 460 nm
  - Gain set to 82.5% for 5 mM 2-Naphthol
- Reads baselined to empty vector control



# EREDs – Phenolic preparation



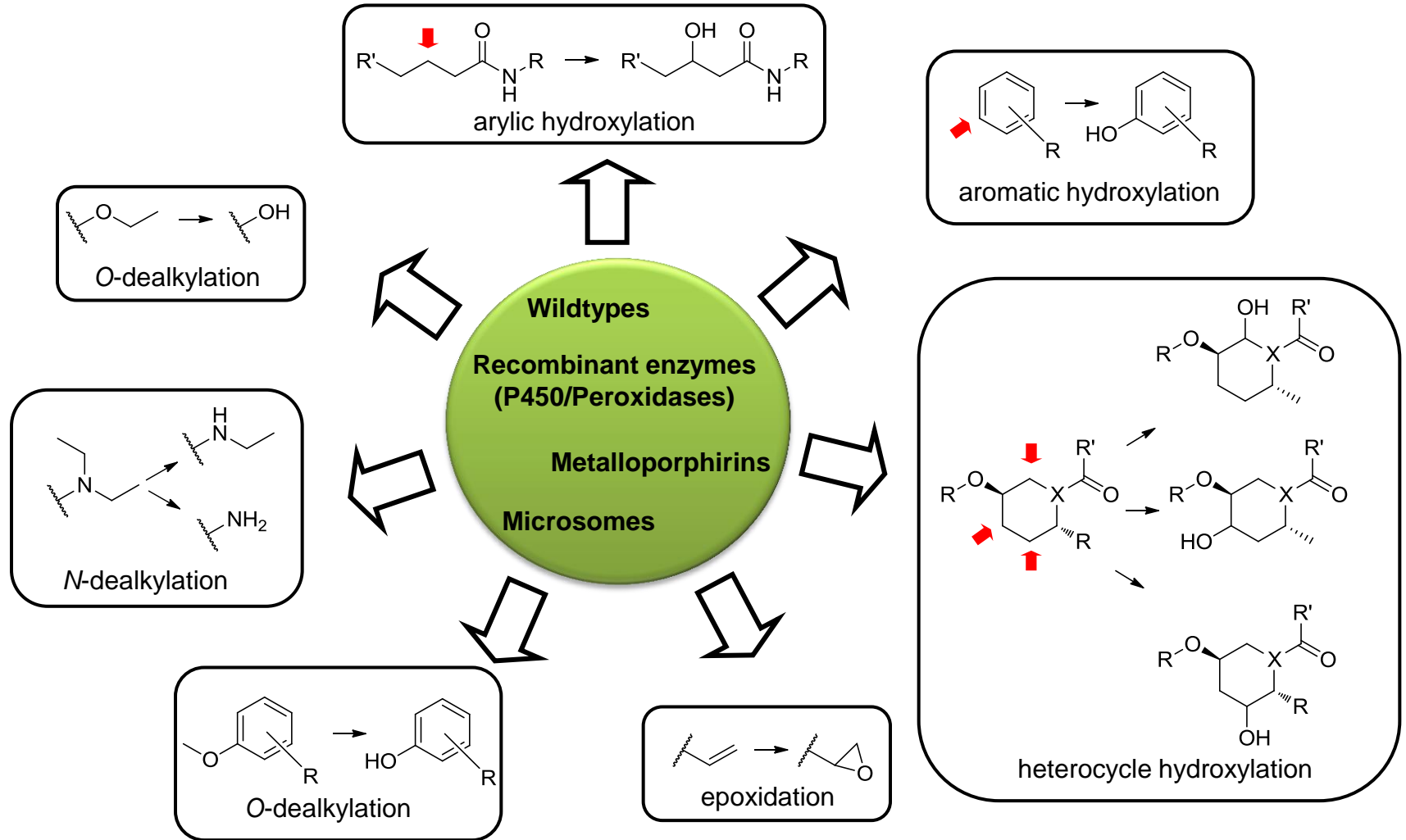
## ERED - E9





# P450 enzymes

# 24 Biooxidation



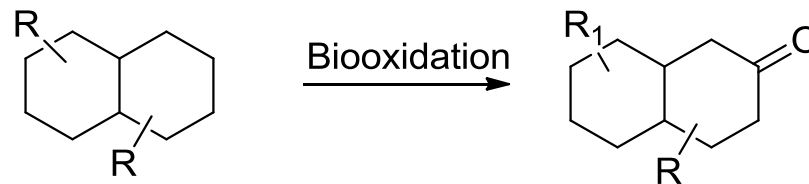


# Biooxidation



## Customer project

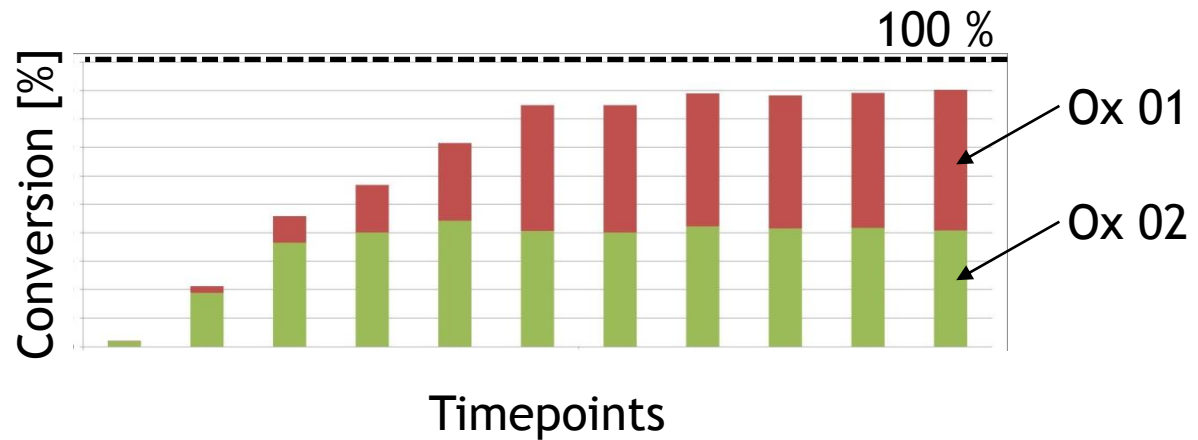
- P450 project
- Enzyme screening and hit ID, enzyme engineering
- Reaction optimisation and scale up from 100 mL to 100 L to 1m<sup>3</sup>
- Reaction engineering





## Two Step P450 Oxidation

Terpenoid → Oxidation Product 1 → Oxidation product 2

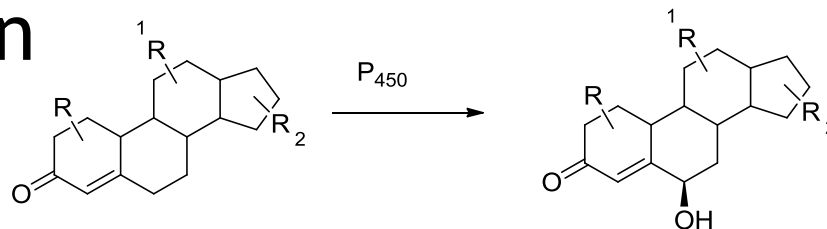


- P450 reaction scaled up to 100 L
- Isolation of ~ 100g desired oxidation products
- NADPH recycling system used
- 1 m<sup>3</sup> scale-up successful
- Next scale 6m<sup>3</sup> in a chemical reactor

- Fermentation for catalyst supply - 15m<sup>3</sup>

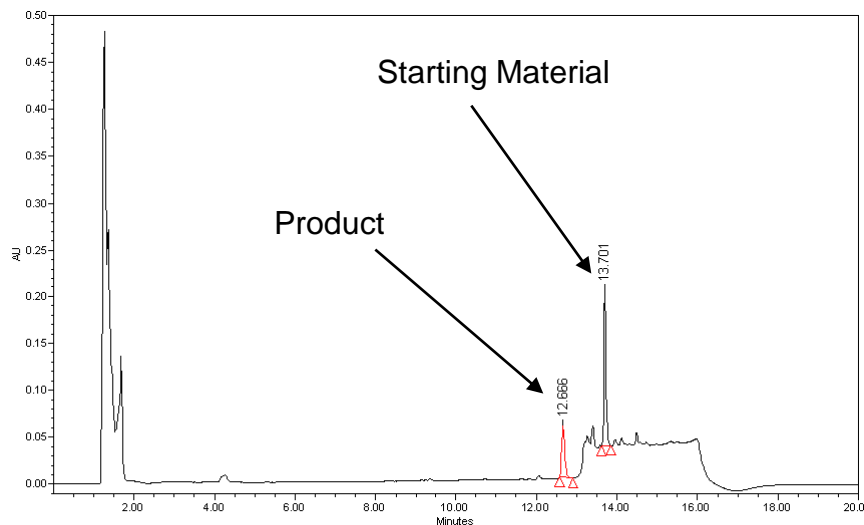


## P450 Oxidation



### Modular Project Deliverables

- P<sub>450</sub> and Streptomet™ screen
- Active P<sub>450</sub> identified
- P<sub>450</sub> ALM-CYP18 identified
- Evolution underway
- **Biooxidation scaled to 5 L in a fermenter**

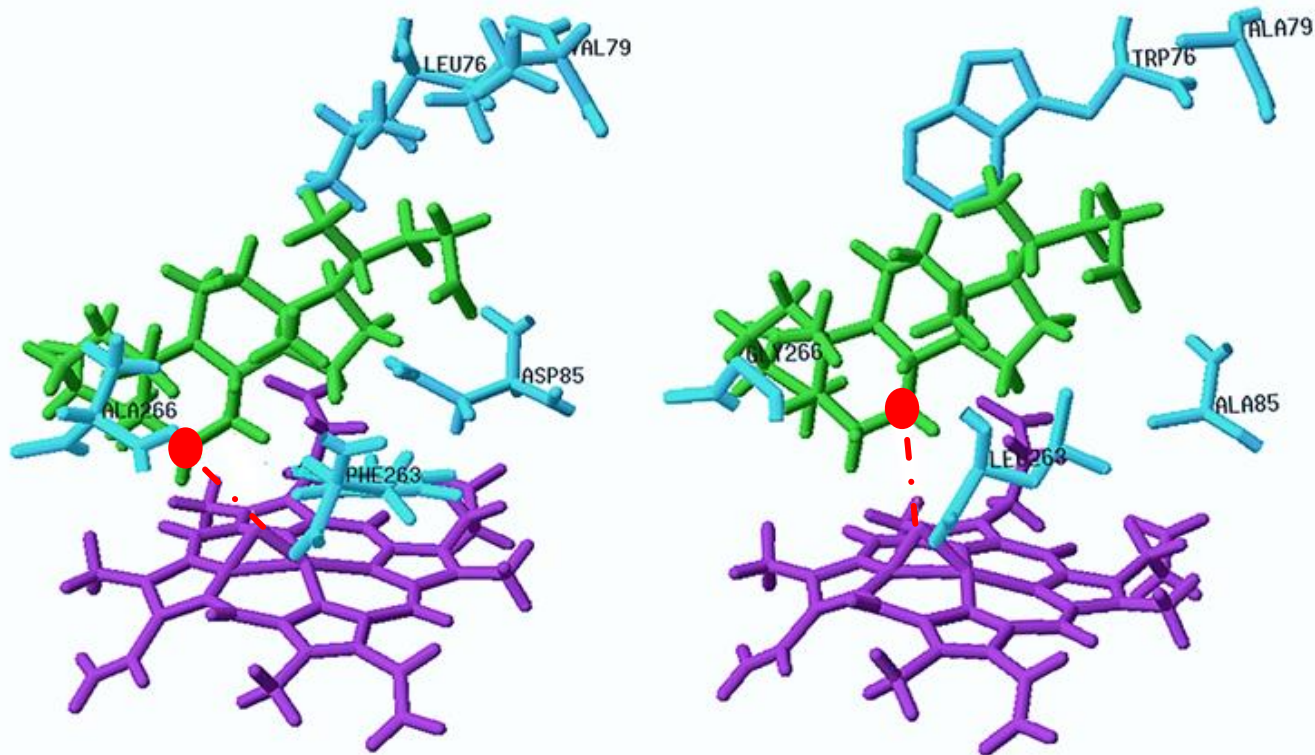
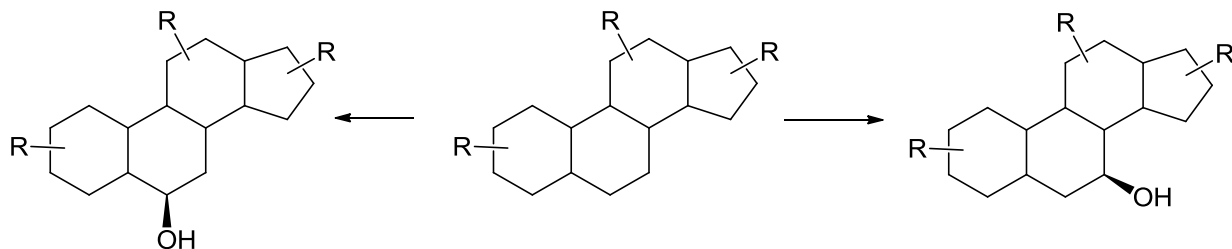


# Biooxidation



## P450 Oxidation - Molecular modelling

Leu → Try





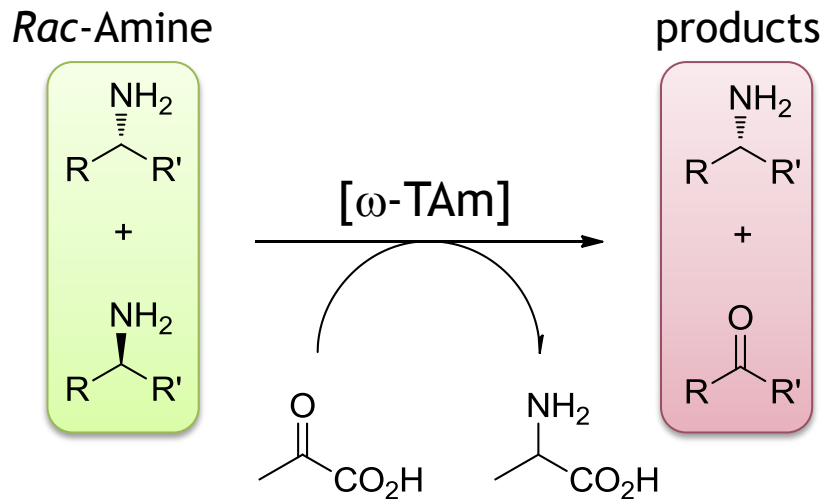
# TAm enzymes

# Transaminase



## Preparation of enantio-enriched $\alpha$ -chiral primary amines

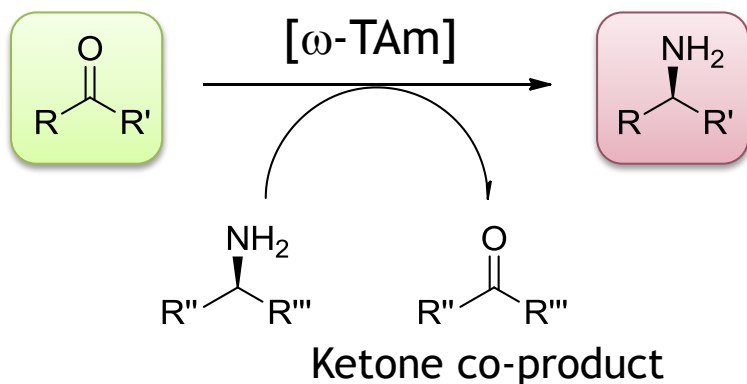
### a) Kinetic resolution



a) Kinetic resolution starting with racemic amines (limited by 50% yield)

### b) Asymmetric synthesis

prochiral ketone

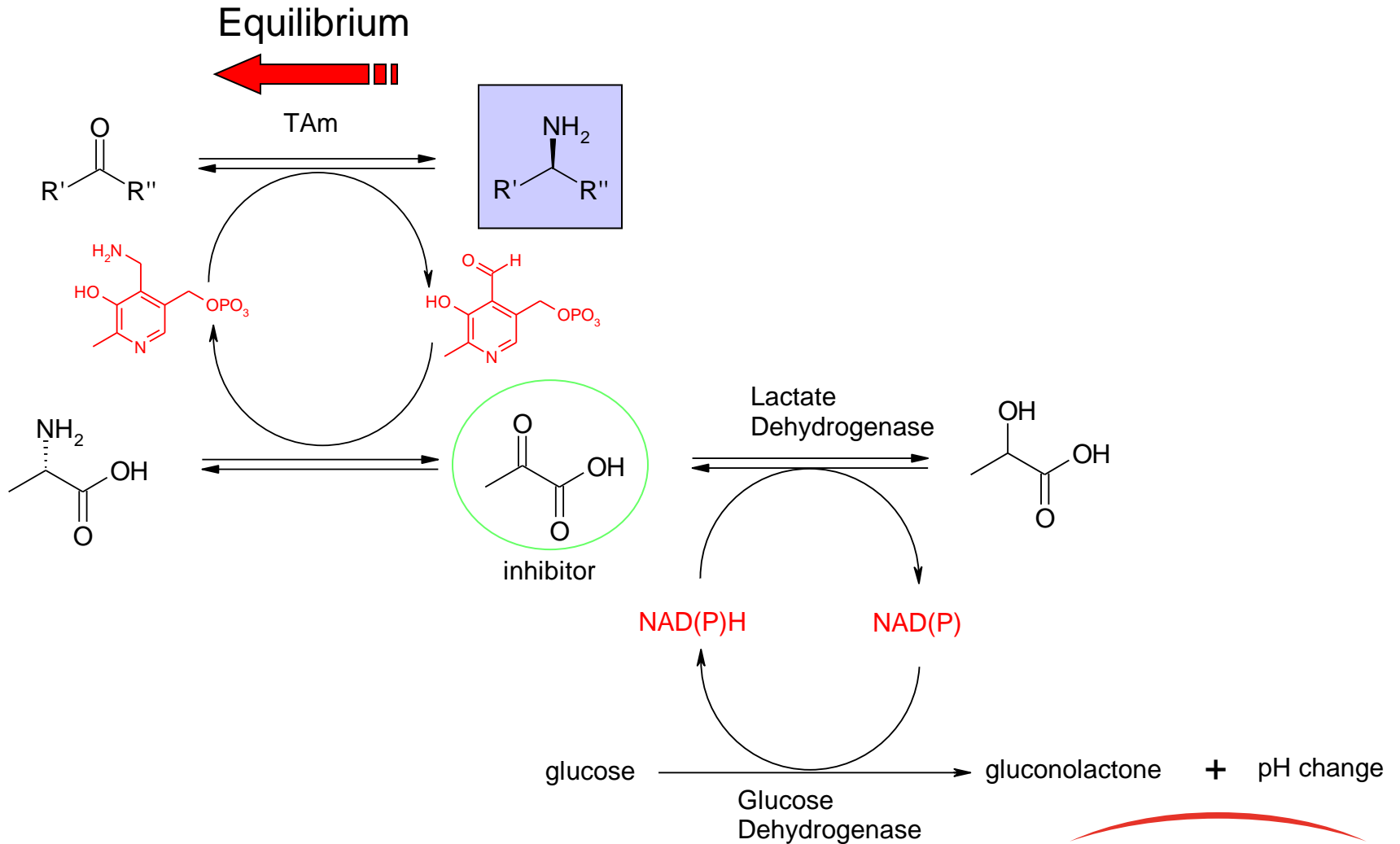


b) Asymmetric synthesis of prochiral ketones (theoretically 100% yield possible)

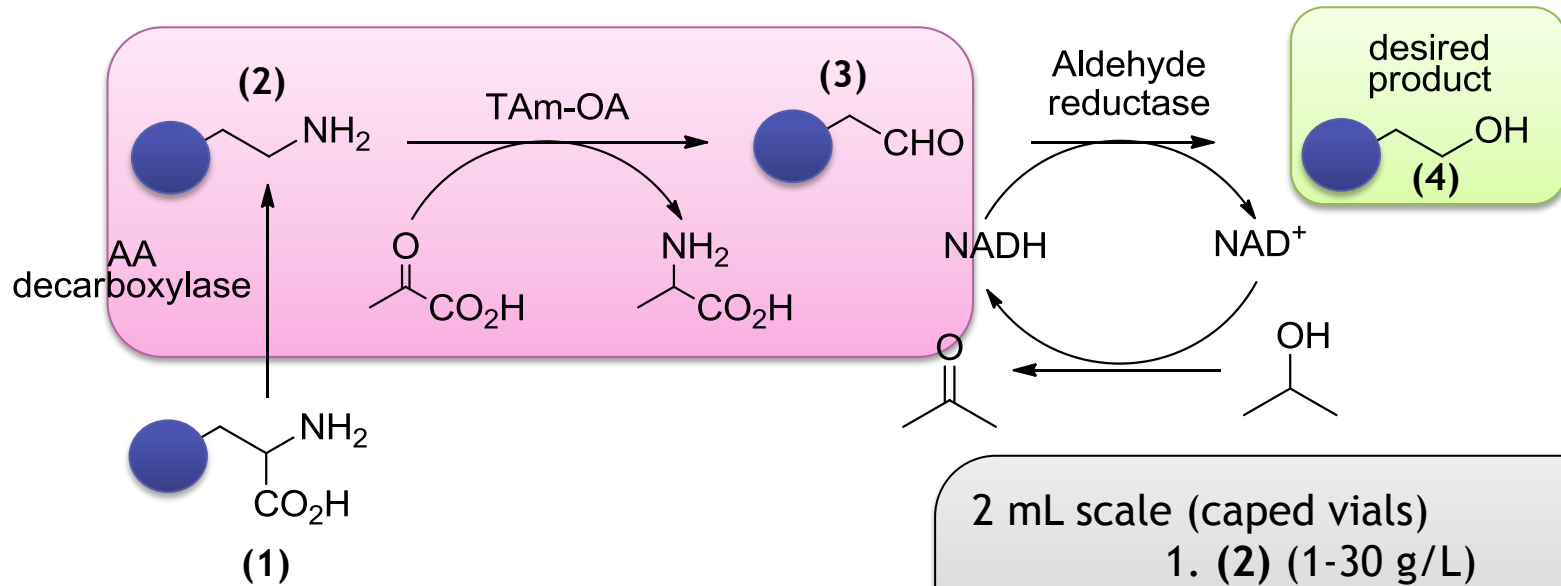
# Transaminase



Strategy used at Almac to remove inhibitory side products



# Transaminase - Cascade



2 mL scale (caped vials)

- (2) (1-30 g/L)
- (3) (0-15 g/L)
- L-Ala (1-50 g/L)
- pyruvic acid (5-200 mM)

pH 7.4 (adjusted before reaction)

## Conclusion

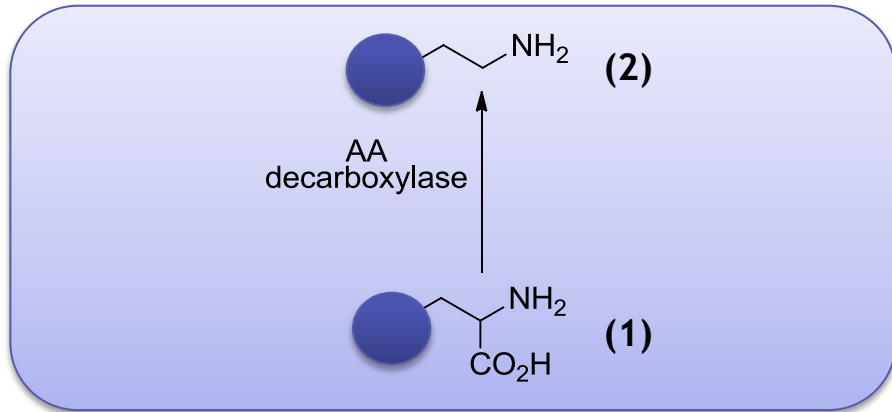
- TAm is active with substrate (2) (5-30 g/L)
- Inhibition with L-alanine (70 % residual activity at 10 g/L), and pyruvic acid (75 % residual activity at 50 mM)
- TAm - maximum apparent specific activity 0.35 U/mg<sub>CFE</sub> (at 30 g/L substrate (2)), and 0.1 U/mg<sub>CFE</sub> (at 7 g/L substrate (2))



# Transaminase - Cascade



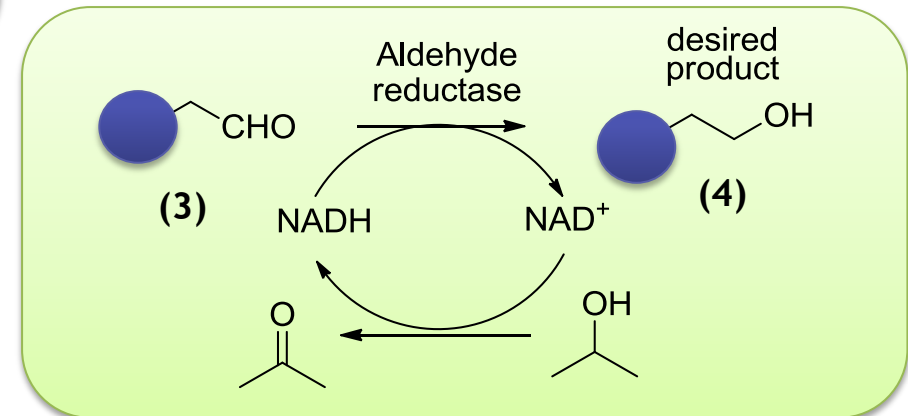
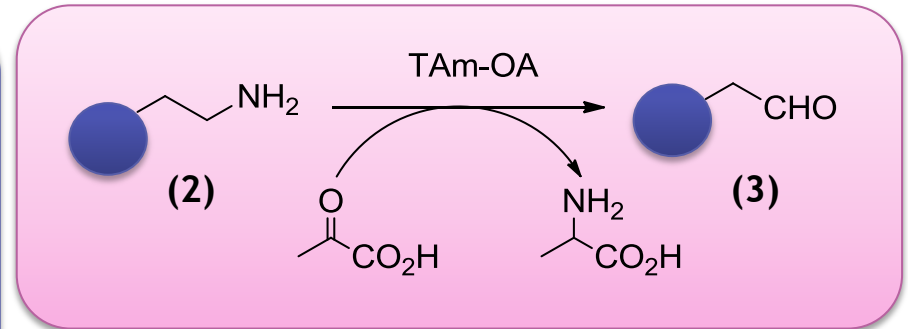
## Step 1



5 g scale, 25 g/L L-AA  
open vessel with pH control  
10 % enz, 0.04 % PLP, pH 7.4, 63%  
conversion in 42 h

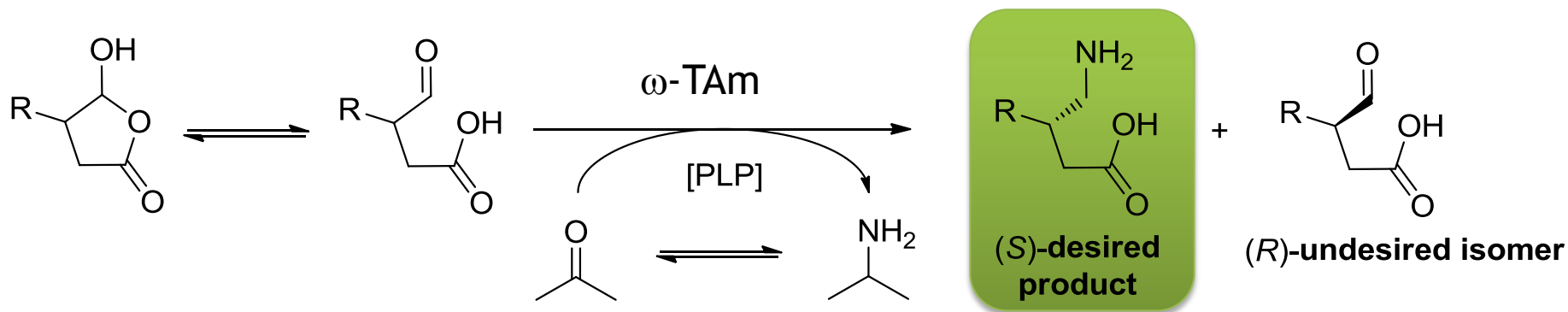
5 g scale, 25 g/L L-AA  
Closed vessel, no pH control  
20 % enz, 0.04% PLP,  
pH 7.14 (initial), pH 7.54 (final)  
97% conversion by HPLC in 18 h

## Step 2 and 3



Drop-wise addition of (2) and pyruvic acid with pH control and (3) - 5 g reaction completed in 16 h

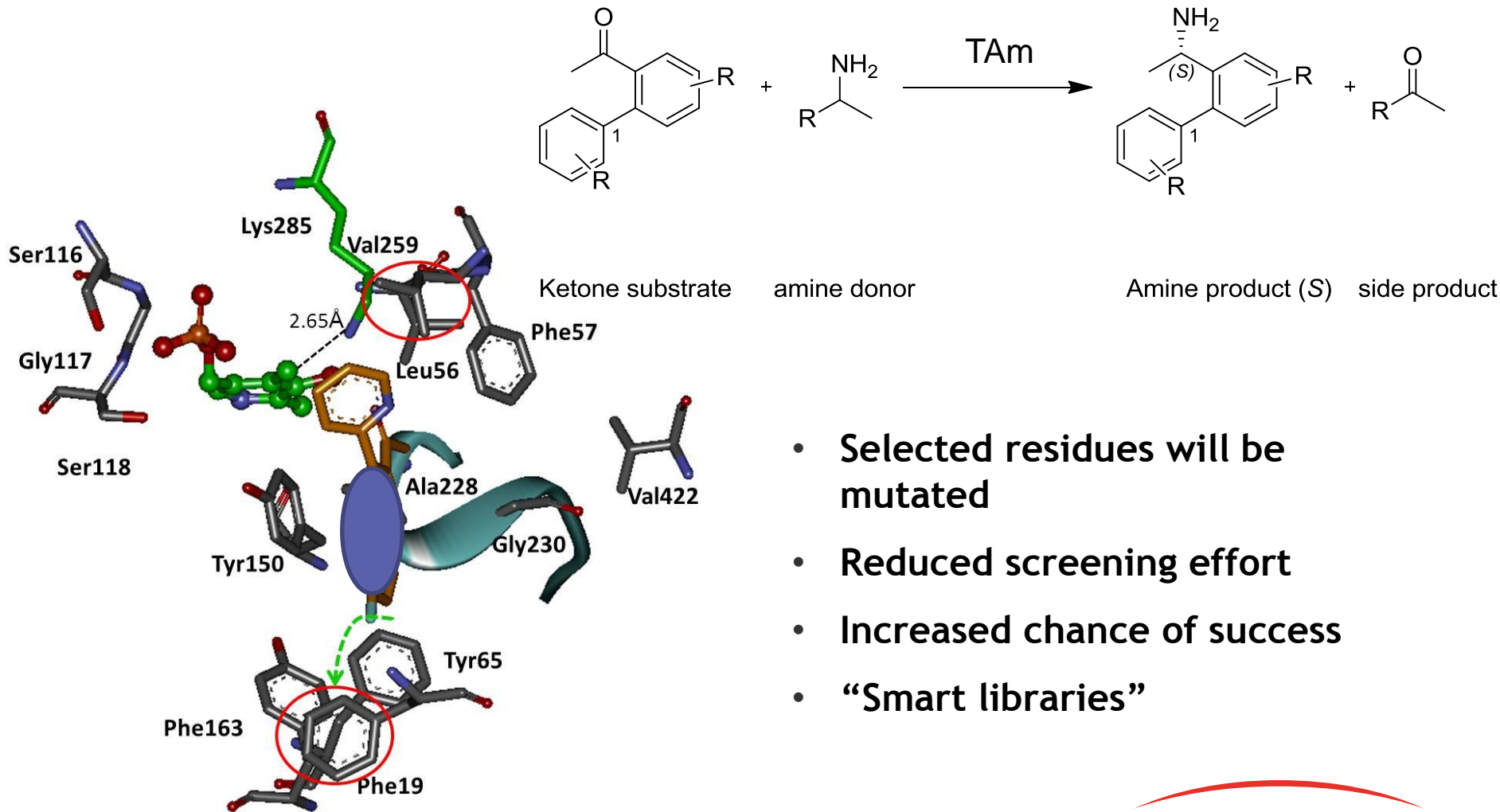
# Transaminase - DKTAm



- Project Aim:
  - process optimisation of the transamination to afford quantitative yield while maintaining ee of >95%
  - Development of a DKTAm
  - TAm immobilised

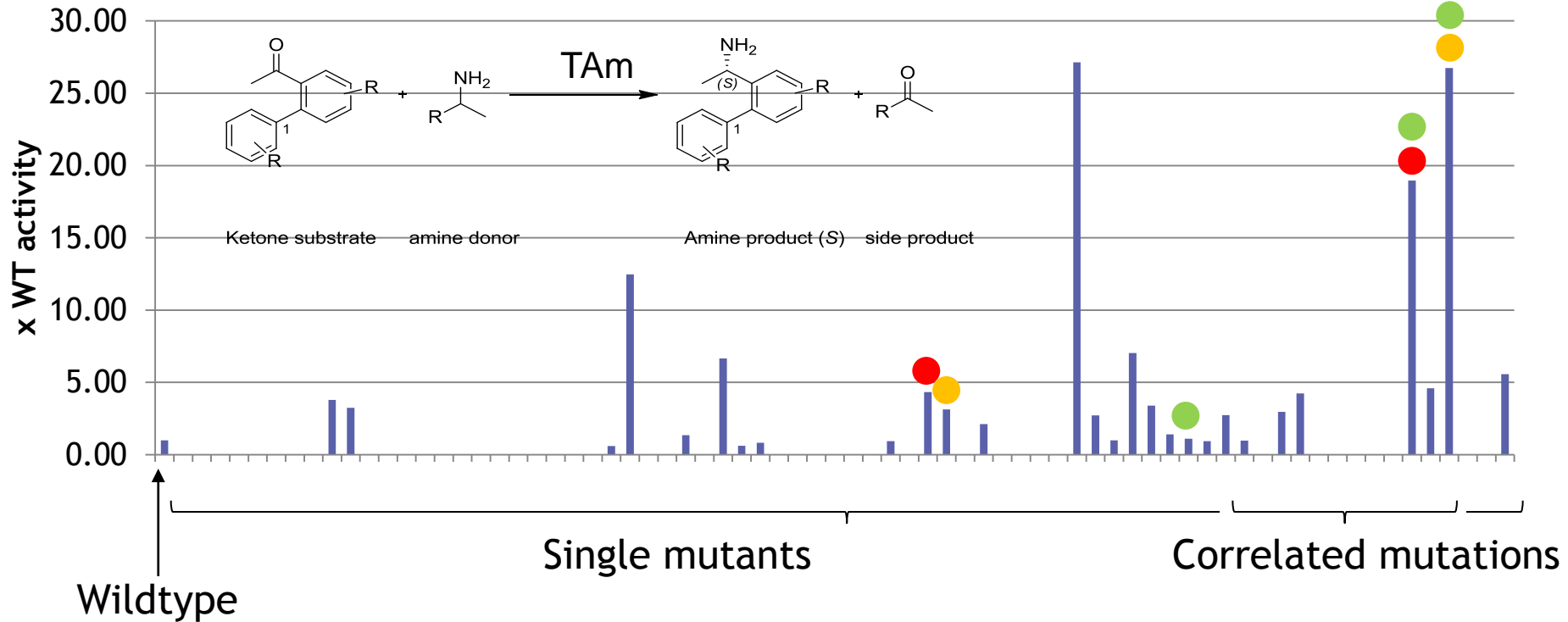


## Substrate specific mutagenesis by protein modelling





## Combination of techniques



⇒ 72 Mutants screened => first round improvement: 25 x wildtype reaction



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Received 13th August 2015, Accepted 23rd September 2015

# A rapid, sensitive colorimetric assay for the high-throughput screening of transaminases in liquid or solid-phase†

D. Baud,<sup>a</sup> N. Ladkau,<sup>a</sup> T. S. Moody,<sup>b</sup> J. M. Ward<sup>c</sup> and H. C. Hailes<sup>\*a</sup>

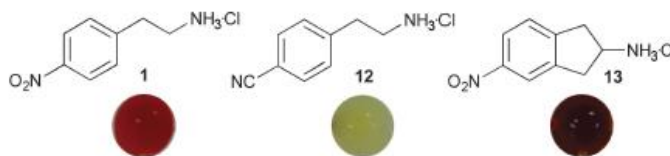
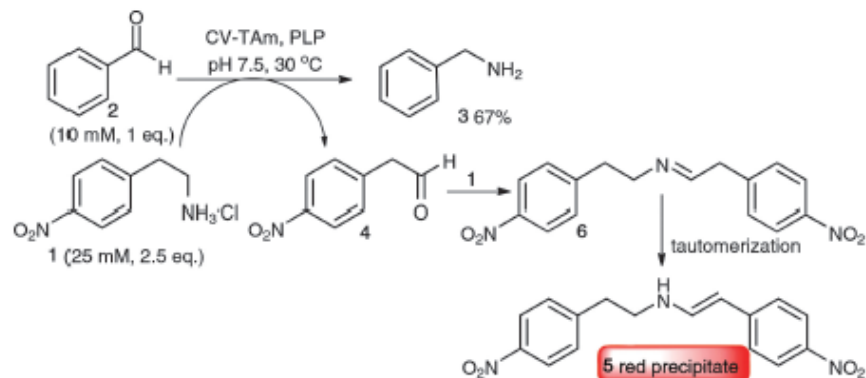
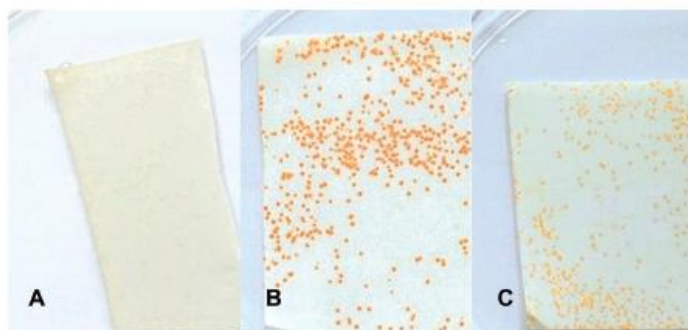
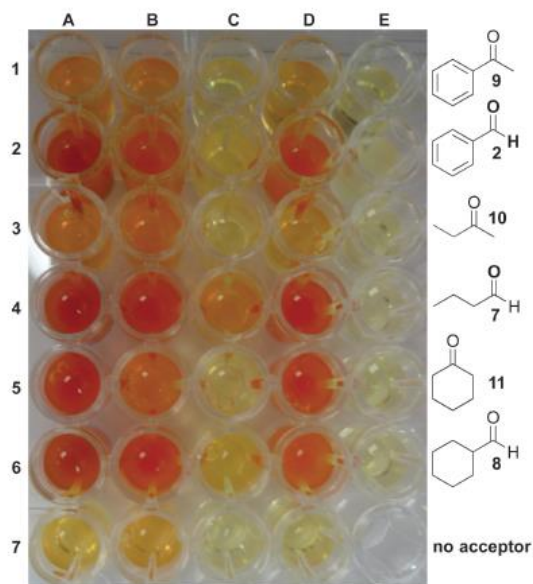


Fig. 2 Assay coloration when using amino donors **1**, **12** and **13** with CV-TAm and acceptor **7**.



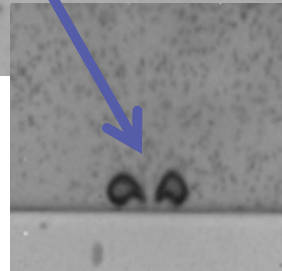
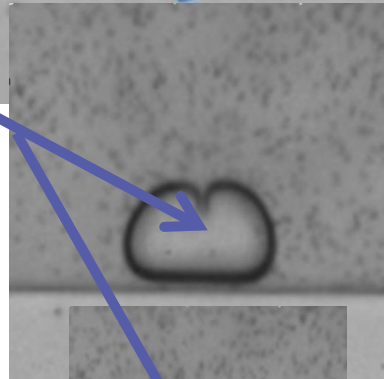
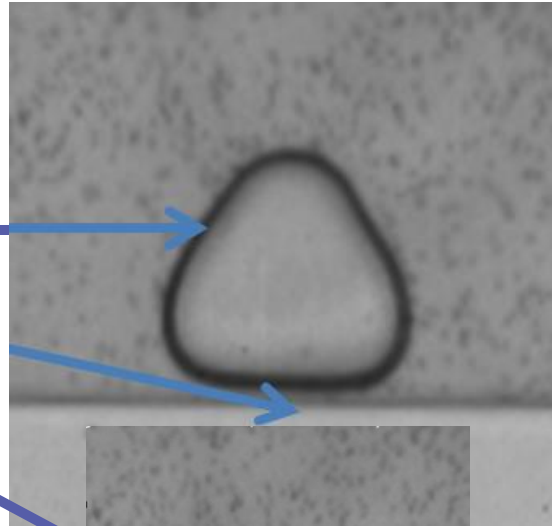


# US process intensification

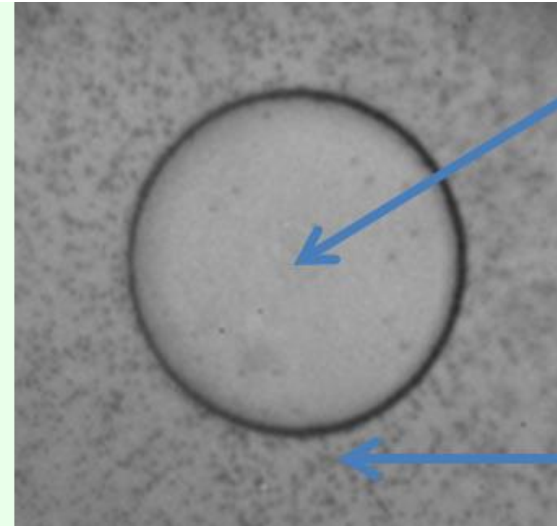


Acknowledgement Prof. T Mason, Uni. of Coventry

**UNSYMMETRIC COLLAPSE**  
Inrush of liquid from one side of the collapsing bubble produces powerful jet of liquid targeted at surface



- Lignocellulose, cell, algae weakening
- (Bio)polymer degradation
- Crystallization
- Cell permeation
- Emulsification



*IN THE CAVITY*  
extreme conditions on collapse 5000°C and 2000 atmospheres

*IN THE BULK MEDIA*  
intense shear forces

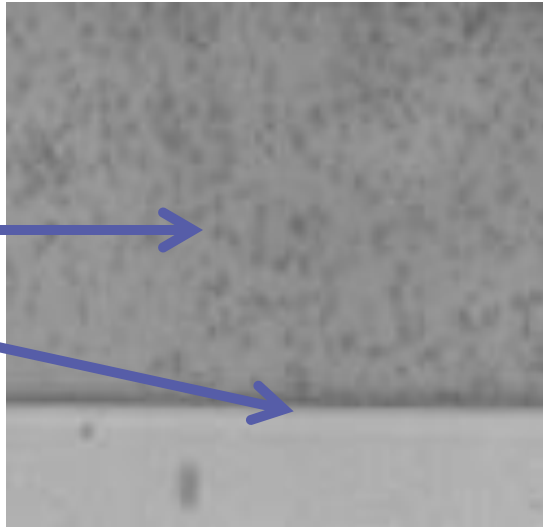
- Lignocellulose, cell algae weakening
- Cell permeation
- Biocatalysis enhancement
- Surface attrition
- Surface activation
- Improved heat/mass transfer
- Emulsification



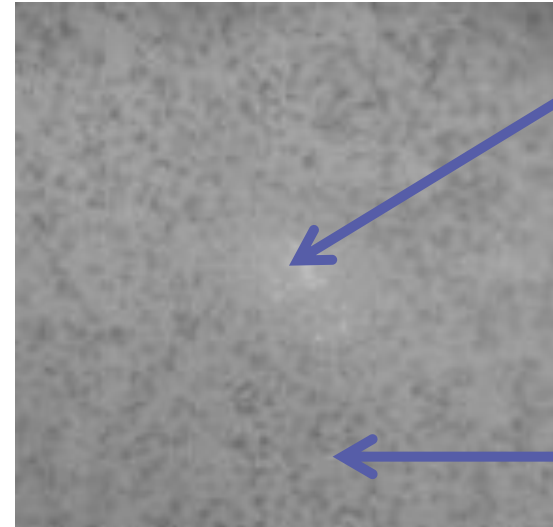
Acknowledgement Prof. T Mason, Uni. of Coventry

## UNSYMMETRIC COLLAPSE

Inrush of liquid from one side of the collapsing bubble produces powerful jet of liquid targeted at surface



- Lignocellulose weakening
- (Bio)polymer degradation
- Crystallization
- Cell permeation



*IN THE CAVITY*  
extreme conditions on collapse 5000°C and 2000 atmospheres

*IN THE BULK MEDIA*  
intense shear forces

- Lignocellulose weakening
- Cell permeation
- Biocatalysis enhancement
- Surface attrition
- Surface activation
- Improved heat/mass transfer

Video courtesy of University of Twente, Netherlands.  
and Shimadzu Europa GmbH, Duisburg, Germany





Temperature 0 to 70°C

50W - ~ 5 kW  
Depending on  
main reactor  
vol. & power  
reqd.

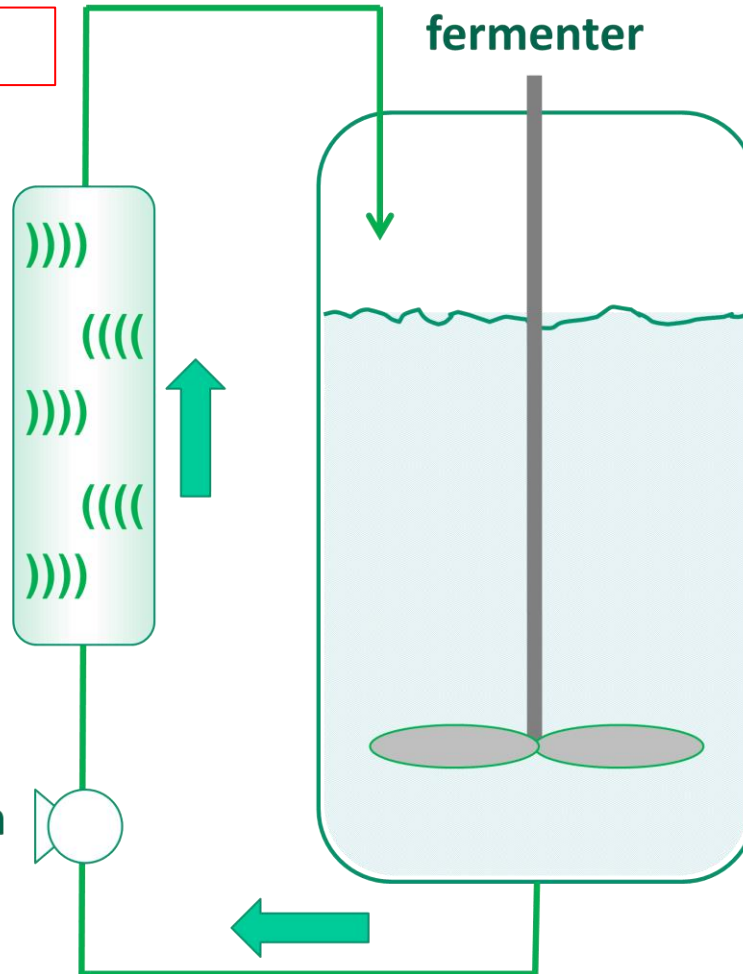
Power  
Efficient  
Ultrasonic  
module(s)

Recirculation  
10 - 100  
L/min

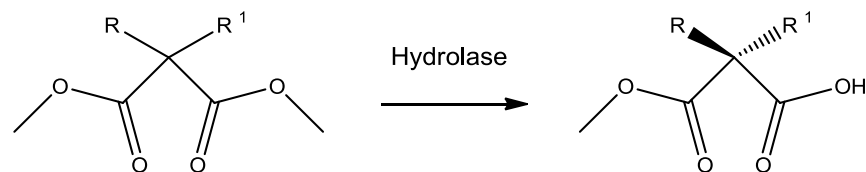
Recirculation  
pump

Bioreactor /  
fermenter

Reactor 50 -  
5000 L

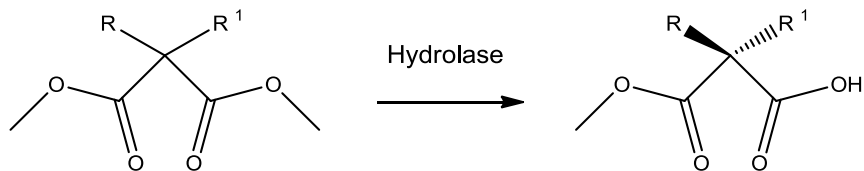


# Process intensification

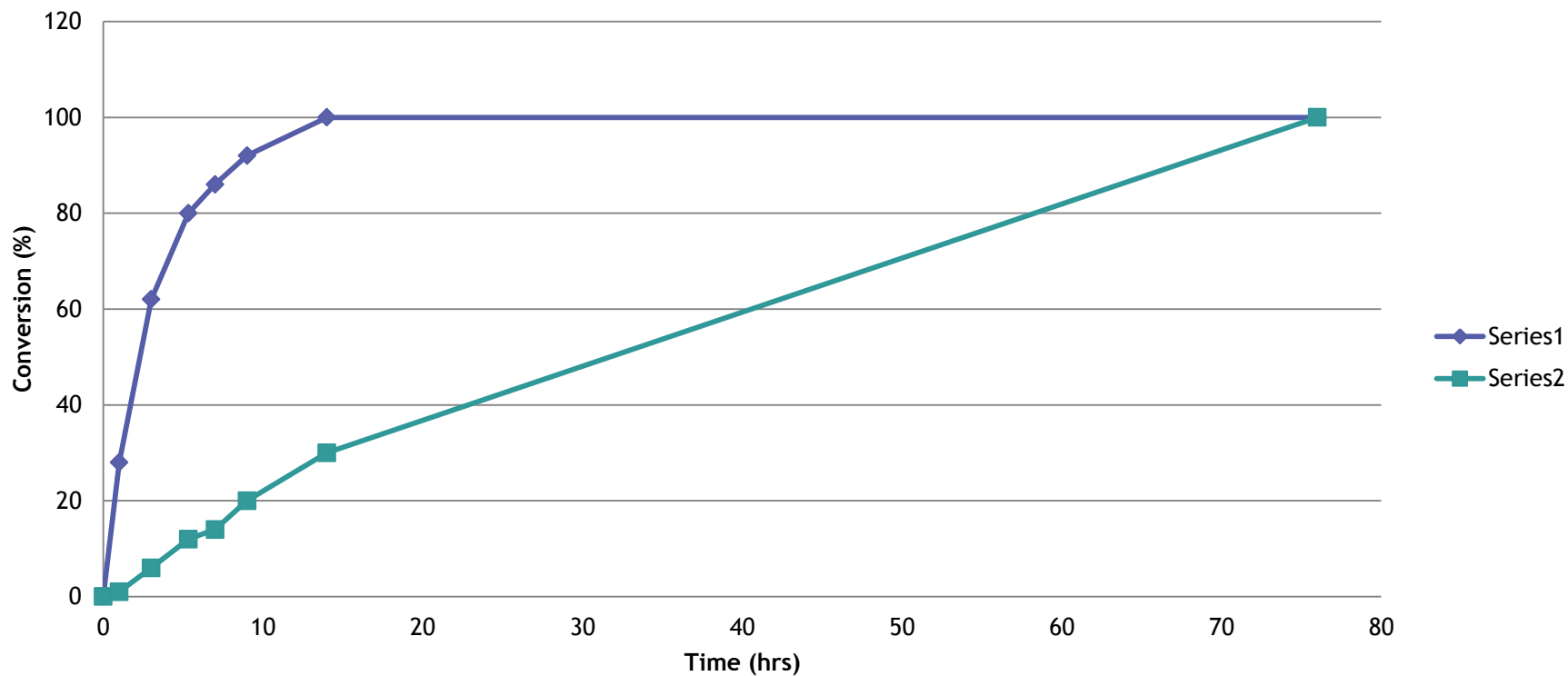


- Process being developed for multi-tonne, Step 2 of a 5 step process
- Process scale-up resulted in mixing problems
- Poor performance for reaction time
- **Options?** Enzyme evolution or Application of US or both

# Process intensification



## Ultrasound assisted biotransformation



# Current technology Configured in reactor / recirculation systems

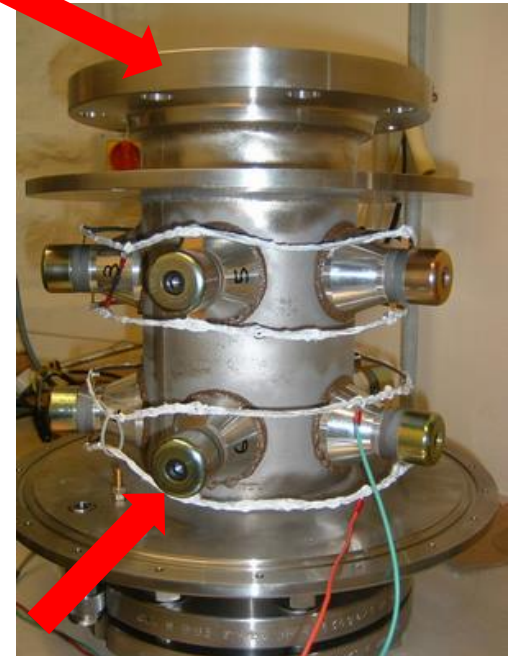


Pictures courtesy of Celbius

Medium out



Flanged cylindrical pipe

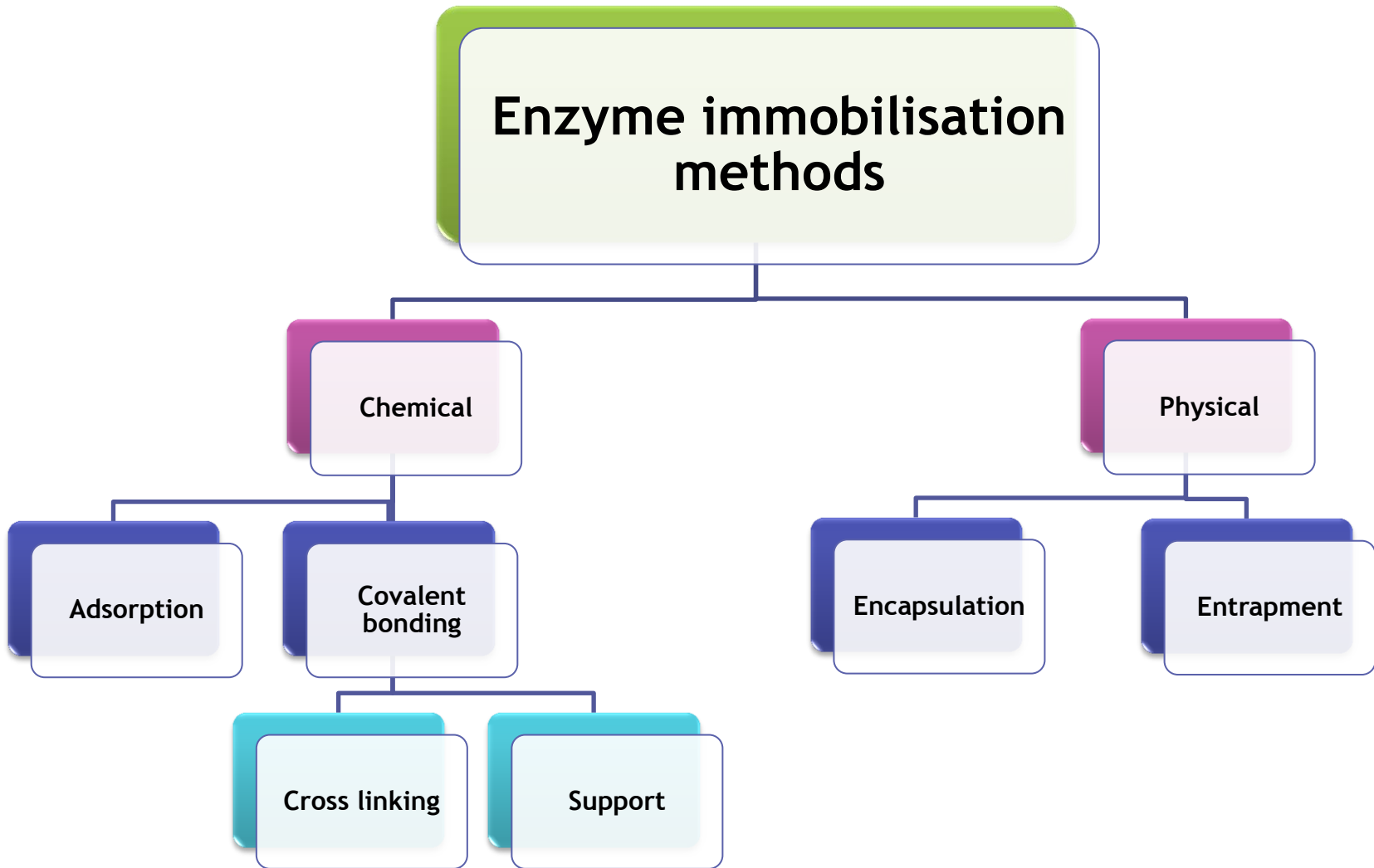


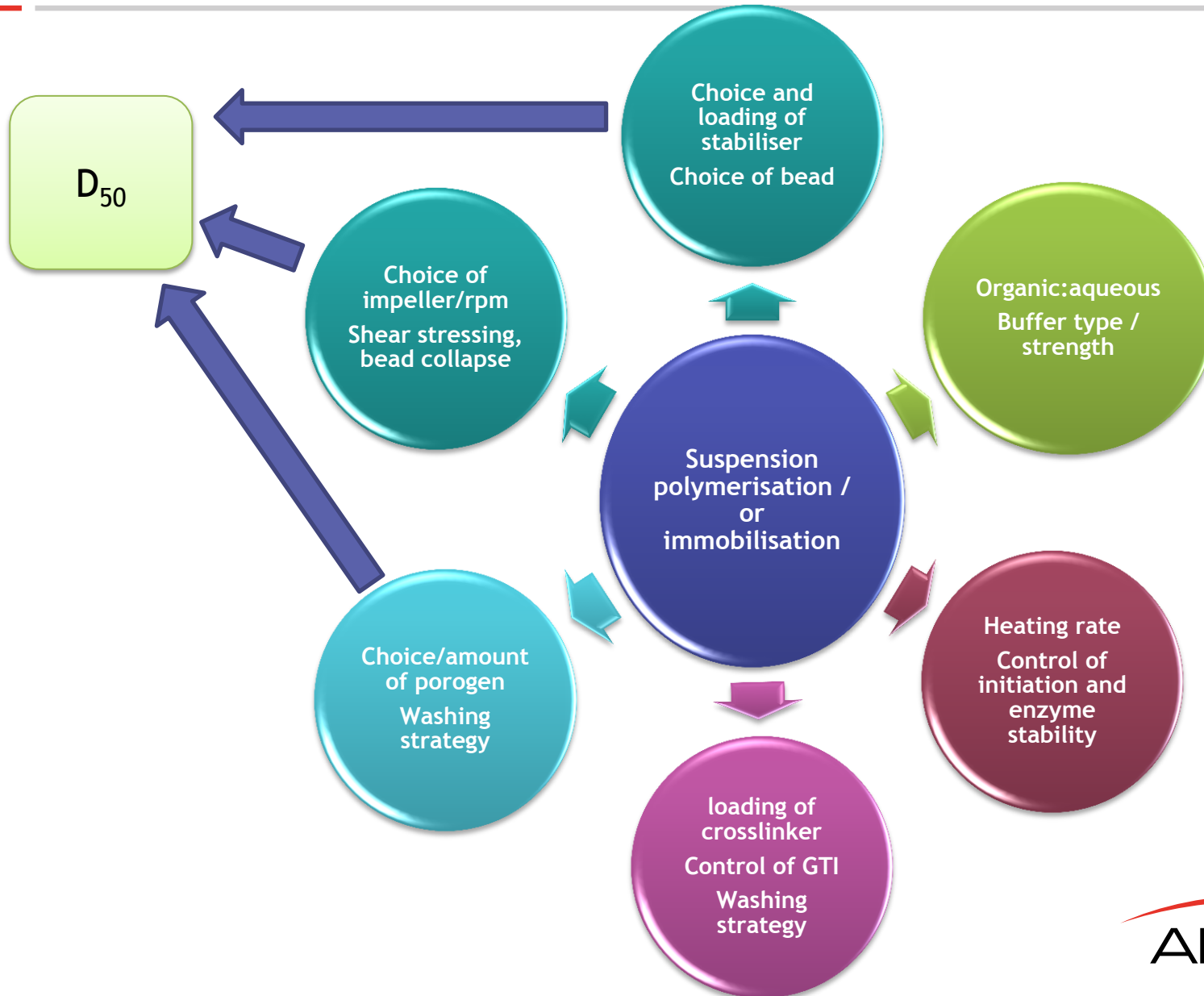
Medium in

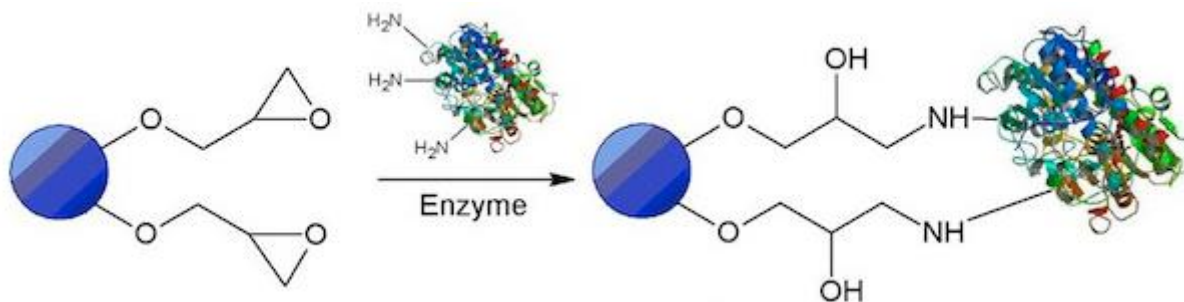
Transducers bonded to deliver ultrasound ALMAC



# Immobilised enzymes







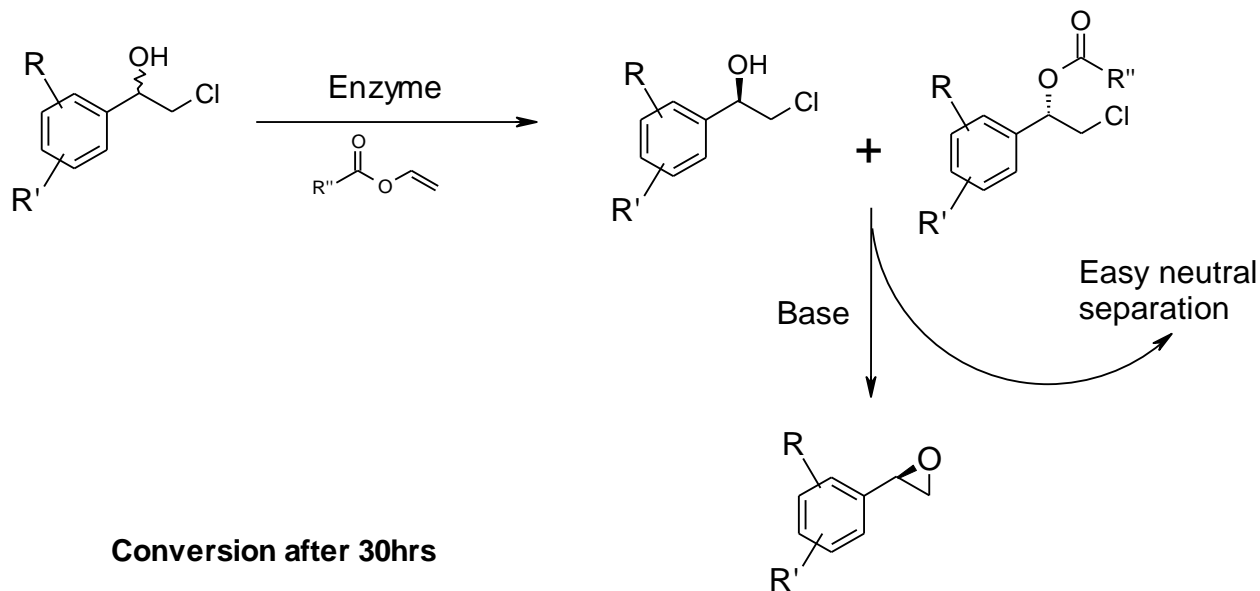
- Optimal for working in biphasic systems or aqueous systems
- Resins are mechanically stable
- Flow systems or CSTR
- Multipoint covalent binding
- Form very stable covalent linkages with different protein groups
- **Enzyme classes immobilised**

Transaminase

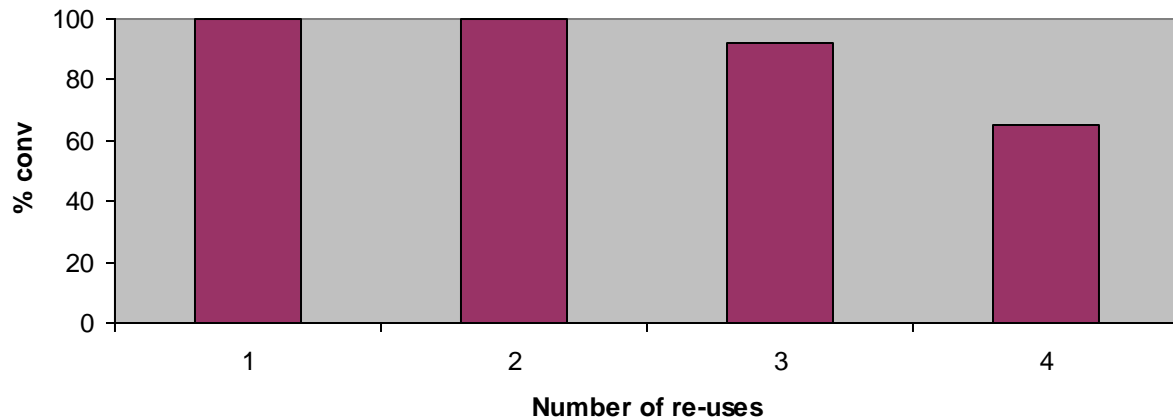
Carbonyl  
reductase

Hydrolase





Conversion after 30hrs



Development:  
 >99 % ee  
 Scale: 450 Kg  
 Manufacture

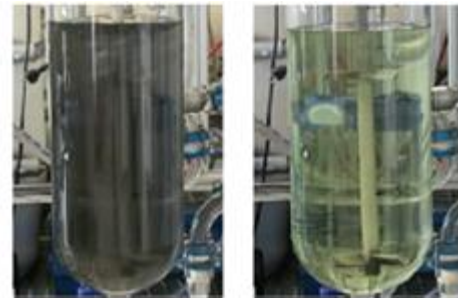
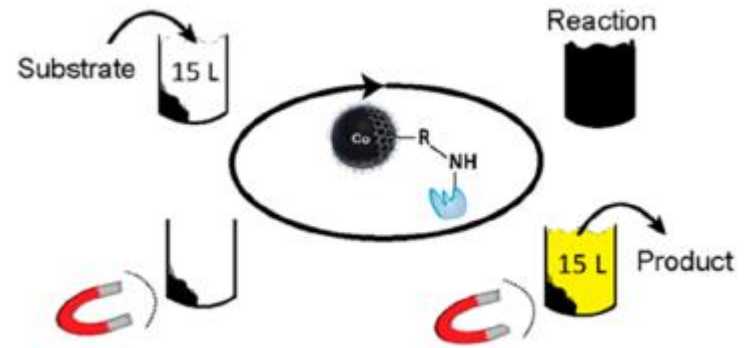


- Enzymes immobilised on carbon coated nanoparticles
  - Metal coated with outer layer
  - Functionalised
  - Enzyme attached

**Ease and quick recovery of immobilised catalyst by use of magnet**

- Enzyme classes immobilised

Hydrolase



Bioconjugate Chem. 2014, 25, 677-684



# API Testing – Enzyme Removal & Detection



## Case Studies Illustrating a Science and Risk-Based Approach to Ensuring Drug Quality When Using Enzymes in the Manufacture of Active Pharmaceutical Ingredients for Oral Dosage Form

Andrew S. Wells,<sup>\*,†</sup> John W. Wong,<sup>||</sup> Peter C. Michels,<sup>||</sup> David A. Entwistle,<sup>‡</sup> Keith Fandrick,<sup>■</sup> Gregory L. Finch,<sup>⊥</sup> Animesh Goswami,<sup>#</sup> Heewon Lee,<sup>■</sup> Stefan Mix,<sup>●</sup> Thomas S. Moody,<sup>●</sup> Long Pang,<sup>‡</sup> Robert K. Sato,<sup>‡</sup> Nicholas J. Turner,<sup>□</sup> and Timothy J. Watson<sup>▽</sup>

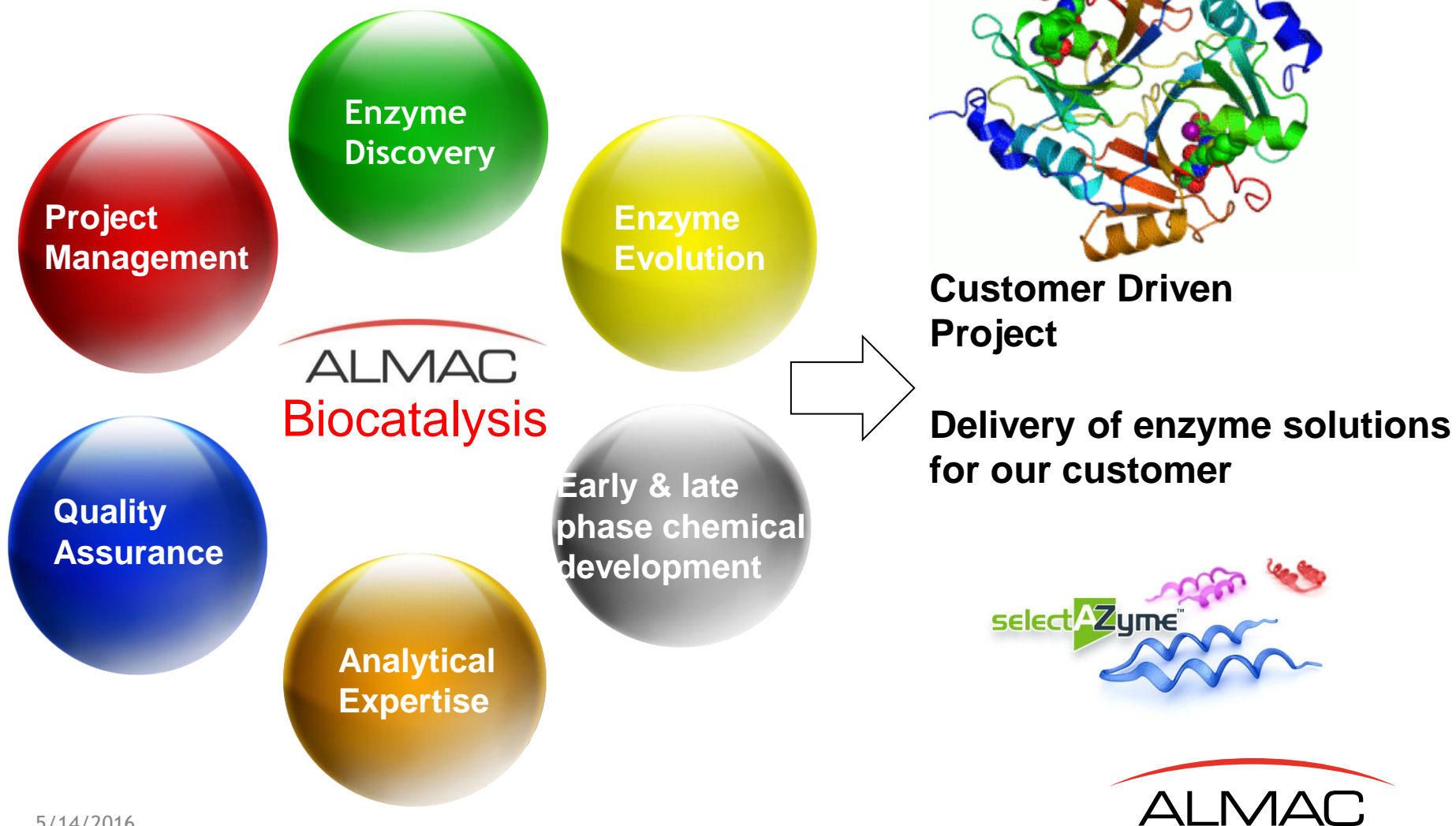
<sup>●</sup>Almac, Department of Biocatalysis and Isotope Chemistry, 20 Seagoe Industrial Estate, Craigavon BT63 5QD, Northern Ireland United Kingdom

Assay	Range	Comment
NanoOrange®	10 ng/mL to 10 µg/mL	Low protein-to-protein signal variability Detection not influenced by reducing agents or nucleic acids
BCA	0.5 µg/mL to 1.5 mg/mL	Samples must be read within 10 minutes Not compatible with reducing agents
Bradford	1 µg/mL to 1.5 mg/mL	Proteins precipitate over time High protein-to-protein signal variability Not compatible with detergents
Lowry	1 µg/mL to 1.5 mg/mL	Lengthy, multistep procedure Not compatible with detergents, carbohydrates or reducing agents
Absorbance at 280 nm	50 µg/mL to 2 mg/mL	High protein-to-protein signal variability Detection influenced by nucleic acids and other residues



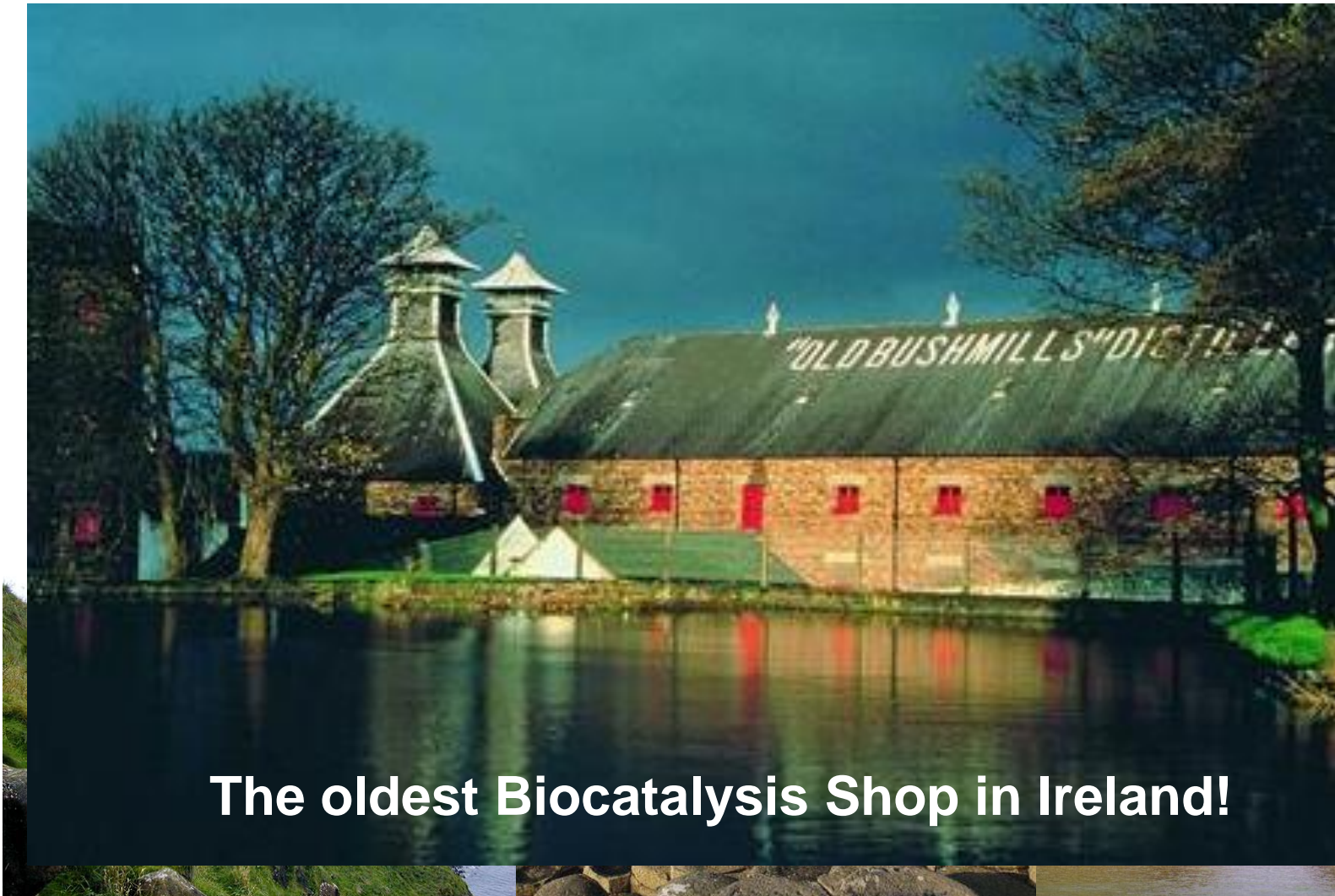
	Example 3: API 3	Example 4: API 4	Example 5: API5	Example 6: API 6
Enzymatic step	Pre RSM, C-C bond formation	Pre RSM, ketone reduction	Post RSM, Alcohol oxidation	Pre RSM Ketone Reduction
Stage in synthesis	Several steps before API	Several steps before API	Penultimate step	Several steps before API
Enzyme type	Enzyme (Cells from E. coli fermentation)	KRED (liquid formulation from in E. coli fermentation)	KRED (whole cell formulation produced in Gluconobacter oxydans)	KRED (Dry powder produced from E. coli fermentation)
Control strategy	Test for total proteins, DNA, endotoxins and microbiological residues; demonstrate fate and purge; no enzyme residue specifications for API	Test for total proteins; no enzyme residue specifications for API	Test for total proteins, DNA, endotoxins and microbiological residues; demonstrate fate and purge; no enzyme residue specifications for API	Test for total proteins; in-process testing; demonstrate fate and purge; no enzyme residue specifications for API

# Biocatalysis and more





# Where we are





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